



## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<b>(51) International Patent Classification <sup>6</sup> :</b> <b>A61K 9/12, 9/00, 9/16, 47/48, 47/14, 38/28, 38/23, 38/09, 31/135</b>	<b>A1</b>	<b>(11) International Publication Number: WO 98/31346</b>  <b>(43) International Publication Date: 23 July 1998 (23.07.98)</b>
<b>(21) International Application Number: PCT/US97/20930</b>  <b>(22) International Filing Date: 17 November 1997 (17.11.97)</b>  <b>(30) Priority Data:</b> 784,421                      16 January 1997 (16.01.97)      US 60/059,004                15 September 1997 (15.09.97)      US  <b>(71) Applicants: MASSACHUSETTS INSTITUTE OF TECHNOLOGY [US/US]; 11 Massachusetts Avenue, Cambridge, MA 02139 (US). THE PENN STATE RESEARCH FOUNDATION [US/US]; 207 Old Main, University Park, PA 16802 (US).</b>  <b>(72) Inventors: EDWARDS, David, A.; 109 Hartswick Avenue, State College, PA 16803 (US). HANES, Justin; 223 Brandon Road, Baltimore, MD 21212 (US). EVORA, Carmen; 22 Isaac Albeniz Street, E-38208 La Laguna (ES). LANGER, Robert, S.; 77 Lombard Street, Newton, MA 02158 (US). VANBEVER, Rita; 11 Centre Street #3, Cambridge, MA 02139 (US). MINTZES, Jeffrey; Apartment #A-12, 421 E. Beaver Avenue, State College, PA 16801 (US). WANG, Jue; 869 Southgate Drive, State College, PA 16801 (US). CHEN, Donghao; 1013 South Allen Street #408, State College, PA 16801 (US).</b>		<b>(74) Agent: PABST, Patrea, L.; Arnall Golden &amp; Gregory, LLP, 2800 One Atlantic Center, 1201 West Peachtree Street, Atlanta, GE 30309-3450 (US).</b>  <b>(81) Designated States: CA, JP, European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).</b>  <b>Published</b> <i>With international search report.</i> <i>With amended claims.</i>
<b>(54) Title: PREPARATION OF PARTICLES FOR INHALATION</b>  <b>(57) Abstract</b>  <p>Particles incorporating a surfactant and/or a hydrophilic or hydrophobic complex of a positively or negatively charged therapeutic agent and a charged molecule of opposite charge for drug delivery to the pulmonary system, and methods for their synthesis and administration are provided. In a preferred embodiment, the particles are made of a biodegradable material and have a tap density less than 0.4 g/cm<sup>3</sup> and a mass mean diameter between 5 μm and 30 μm, which together yield an aerodynamic diameter of the particles of between approximately one and three microns. The particles may be formed of biodegradable materials such as biodegradable polymers. For example, the particles may be formed of poly(lactic acid) or poly(glycolic acid) or copolymers thereof. Alternatively, the particles may be formed solely of a therapeutic or diagnostic agent and a surfactant. Surfactants can be incorporated on the particle surface for example by coating the particle after particle formation, or by incorporating the surfactant in the material forming the particle prior to formation of the particle. Exemplary surfactants include phosphoglycerides such as dipalmitoyl phosphatidylcholine (DPPC). The particles can be effectively aerosolized for administration to the respiratory tract to permit systemic or local delivery of wide a variety of therapeutic agents. Formation of complexes of positively or negatively charged therapeutic agents with molecules of opposite charge can allow control of the release rate of the agents into the blood stream following administration.</p>		

## PREPARATION OF PARTICLES FOR INHALATION

### Background of the Invention

The present application relates generally to particles for use in drug delivery to the pulmonary system.

5           Aerosols for the delivery of therapeutic agents to the respiratory tract have been described, for example, Adjei, A. and Garren, J. *Pharm. Res.*, 7: 565-569 (1990); and Zanen, P. and Lamm, J.-W.J. *Int. J. Pharm.*, 114: 111-115 (1995). The respiratory tract encompasses the upper airways, including the oropharynx and larynx, followed by the  
10   lower airways, which include the trachea followed by bifurcations into the bronchi and bronchioli. The upper and lower airways are called the conducting airways. The terminal bronchioli then divide into respiratory bronchioli which then lead to the ultimate respiratory zone, the alveoli, or deep lung. Gonda, I. "Aerosols for delivery of therapeutic and diagnostic  
15   agents to the respiratory tract," in *Critical Reviews in Therapeutic Drug Carrier Systems*, 6:273-313 (1990). The deep lung, or alveoli, are the primary target of inhaled therapeutic aerosols for systemic drug delivery.

Inhaled aerosols have been used for the treatment of local lung disorders including asthma and cystic fibrosis (Anderson *et al.*, *Am. Rev. Respir. Dis.*, 140: 1317-1324 (1989)) and have potential for the systemic  
20   delivery of peptides and proteins as well (Patton and Platz, *Advanced Drug Delivery Reviews*, 8:179-196 (1992)). However, pulmonary drug delivery strategies present many difficulties for the delivery of macromolecules; these include protein denaturation during aerosolization, excessive loss of inhaled drug in the oropharyngeal cavity (often  
25   exceeding 80%), poor control over the site of deposition, lack of reproducibility of therapeutic results owing to variations in breathing patterns, the frequent too-rapid absorption of drug potentially resulting in local toxic effects, and phagocytosis by lung macrophages.

Considerable attention has been devoted to the design of therapeutic aerosol inhalers to improve the efficiency of inhalation therapies. Timsina *et. al.*, *Int. J. Pharm.*, 101: 1-13 (1995); and Tansey, I.P., *Spray Technol. Market*, 4: 26-29 (1994). Attention has also been  
5 given to the design of dry powder aerosol surface texture, regarding particularly the need to avoid particle aggregation, a phenomenon which considerably diminishes the efficiency of inhalation therapies. French, D.L., Edwards, D.A. and Niven, R.W., *J. Aerosol Sci.*, 27: 769-783 (1996). Dry powder formulations ("DPFs") with large particle size have  
10 improved flowability characteristics, such as less aggregation (Visser, J., *Powder Technology* 58: 1-10 (1989)), easier aerosolization, and potentially less phagocytosis. Rudt, S. and R.H. Muller, *J. Controlled Release*, 22: 263-272 (1992); Tabata, Y. and Y. Ikada, *J. Biomed. Mater. Res.*, 22: 837-858 (1988). Dry powder aerosols for inhalation therapy are  
15 generally produced with mean diameters primarily in the range of less than 5  $\mu\text{m}$ . Ganderton, D., *J. Biopharmaceutical Sciences*, 3:101-105 (1992); and Gonda, I. "Physico-Chemical Principles in Aerosol Delivery," in *Topics in Pharmaceutical Sciences 1991*, Crommelin, D.J. and K.K. Midha, Eds., Medpharm Scientific Publishers, Stuttgart, pp. 95-  
20 115, 1992. Large "carrier" particles (containing no drug) have been co-delivered with therapeutic aerosols to aid in achieving efficient aerosolization among other possible benefits. French, D.L., Edwards, D.A. and Niven, R.W., *J. Aerosol Sci.*, 27: 769-783 (1996).

The human lungs can remove or rapidly degrade hydrolytically  
25 cleavable deposited aerosols over periods ranging from minutes to hours. In the upper airways, ciliated epithelia contribute to the "mucociliary escalator" by which particles are swept from the airways toward the mouth. Pavia, D. "Lung Mucociliary Clearance," in *Aerosols and the Lung: Clinical and Experimental Aspects*, Clarke, S.W. and Pavia, D.,  
30 Eds., Butterworths, London, 1984. Anderson *et al.*, *Am. Rev. Respir. Dis.*, 140: 1317-1324 (1989). In the deep lungs, alveolar macrophages are capable of phagocytosing particles soon after their deposition.

- Warheit, M.B. and Hartsky, M.A., *Microscopy Res. Tech.*, 26: 412-422 (1993); Brain, J.D., "Physiology and Pathophysiology of Pulmonary Macrophages," in *The Reticuloendothelial System*, S.M. Reichard and J. Filkins, Eds., Plenum, New York, pp. 315-327, 1985; Dorries, A.M. and Valberg, P.A., *Am. Rev. Resp. Disease* 146: 831-837 (1991); and Gehr, P. et al. *Microscopy Res. and Tech.*, 26: 423-436 (1993). As the diameter of particles exceeds 3  $\mu\text{m}$ , there is increasingly less phagocytosis by macrophages. Kawaguchi, H. et al., *Biomaterials* 7: 61-66 (1986); Krenis, L.J. and Strauss, B., *Proc. Soc. Exp. Med.*, 107: 748-750 (1961); and Rudt, S. and Muller, R.H., *J. Contr. Rel.*, 22: 263-272 (1992). However, increasing the particle size also has been found to minimize the probability of particles (possessing standard mass density) entering the airways and acini due to excessive deposition in the oropharyngeal or nasal regions. Heyder, J. et al., *J. Aerosol Sci.*, 17: 811-825 (1986).
- Local and systemic inhalation therapies can often benefit from a relatively slow controlled release of the therapeutic agent. Gonda, I., "Physico-chemical principles in aerosol delivery," in: *Topics in Pharmaceutical Sciences 1991*, D.J.A. Crommelin and K.K. Midha, Eds., Stuttgart: Medpharm Scientific Publishers, pp. 95-117 (1992).
- Slow release from a therapeutic aerosol can prolong the residence of an administered drug in the airways or acini, and diminish the rate of drug appearance in the bloodstream. Also, patient compliance is increased by reducing the frequency of dosing. Langer, R., *Science*, 249: 1527-1533 (1990); and Gonda, I. "Aerosols for delivery of therapeutic and diagnostic agents to the respiratory tract," in *Critical Reviews in Therapeutic Drug Carrier Systems* 6: 273-313 (1990).

Controlled release drug delivery to the lung may simplify the way in which many drugs are taken. Gonda, I., *Adv. Drug Del. Rev.*, 5: 1-9 (1990); and Zeng, X. et al., *Int. J. Pharm.*, 124: 149-164 (1995).

Pulmonary drug delivery is an attractive alternative to oral, transdermal, and parenteral administration because self-administration is simple, the lungs provide a large mucosal surface for drug absorption, there is no

first-pass liver effect of absorbed drugs, and there is reduced enzymatic activity and pH mediated drug degradation compared with the oral route. Relatively high bioavailability of many molecules, including macromolecules, can be achieved via inhalation. Wall, D.A., *Drug Delivery*, 2: 1-20 (1995); Patton, J. and Platz, R., *Adv. Drug Del. Rev.*, 8: 179-196 (1992); and Byron, P., *Adv. Drug Del. Rev.*, 5: 107-132 (1990). As a result, several aerosol formulations of therapeutic drugs are in use or are being tested for delivery to the lung. Patton, J.S., *et al.*, *J. Controlled Release*, 28: 79-85 (1994); Damms, B. and Bains, W., *Nature Biotechnology* (1996); Niven, R.W., *et al.*, *Pharm. Res.*, 12(9): 1343-1349 (1995); and Kobayashi, S., *et al.*, *Pharm. Res.*, 13(1): 80-83 (1996).

Drugs currently administered by inhalation come primarily as liquid aerosol formulations. However, many drugs and excipients, especially proteins, peptides (Liu, R., *et al.*, *Biotechnol. Bioeng.*, 37: 177-184 (1991)), and biodegradable carriers such as poly(lactide-co-glycolides) (PLGA), are unstable in aqueous environments for extended periods of time. This can make storage as a liquid formulation problematic. In addition, protein denaturation can occur during aerosolization with liquid formulations. Mumenthaler, M., *et al.*, *Pharm. Res.*, 11: 12-20 (1994). Considering these and other limitations, dry powder formulations (DPF's) are gaining increased interest as aerosol formulations for pulmonary delivery. Damms, B. and W. Bains, *Nature Biotechnology* (1996); Kobayashi, S., *et al.*, *Pharm. Res.*, 13(1): 80-83 (1996); and Timsina, M., *et al.*, *Int. J. Pharm.*, 101: 1-13 (1994). However, among the disadvantages of DPF's is that powders of ultrafine particulates usually have poor flowability and aerosolization properties, leading to relatively low respirable fractions of aerosol, which are the fractions of inhaled aerosol that escape deposition in the mouth and throat. Gonda, I., in *Topics in Pharmaceutical Sciences 1991*, D. Crommelin and K. Midha, Editors, Stuttgart: Medpharm Scientific Publishers, 95-117 (1992). A primary concern with many aerosols is

particulate aggregation caused by particle-particle interactions, such as hydrophobic, electrostatic, and capillary interactions. An effective dry-powder inhalation therapy for both short and long term release of therapeutics, either for local or systemic delivery, requires a powder that displays minimum aggregation, as well as a means of avoiding or suspending the lung's natural clearance mechanisms until drugs have been effectively delivered.

There is a need for improved inhaled aerosols for pulmonary delivery of therapeutic agents. There is a need for the development of drug carriers which are capable of delivering the drug in an effective amount into the airways or the alveolar zone of the lung. There further is a need for the development of drug carriers for use as inhaled aerosols which are biodegradable and are capable of controlled release of drug within the airways or in the alveolar zone of the lung. There also is a need for particles for pulmonary drug delivery with improved aerosolization properties.

It is therefore an object of the present invention to provide improved carriers for the pulmonary delivery of therapeutic agents. It is a further object of the invention to provide inhaled aerosols which are effective carriers for delivery of therapeutic agents to the deep lung. It is another object of the invention to provide carriers for pulmonary delivery which avoid phagocytosis in the deep lung. It is a further object of the invention to provide carriers for pulmonary drug delivery which are capable of biodegrading and releasing the drug at a controlled rate. It is yet another object of the invention to provide particles for pulmonary drug delivery with improved aerosolization properties and optimized particle - particle interactions.

### Summary of the Invention

Particles incorporating a surfactant and/or a hydrophilic or hydrophobic complex of a positively or negatively charged therapeutic agent and a charged molecule of opposite charge for delivery of

therapeutic or diagnostic agents to the pulmonary system, and methods for their synthesis and administration, are provided. Exemplary surfactants include naturally occurring phosphatidylcholines, such as dipalmitoylphosphatidylcholine ("DPPC"). Exemplary hydrophilic or hydrophobic complexes include insulin (negatively charged) and protamine (positively charged). In a preferred embodiment, the particles are aerodynamically light particles, which are made of a biodegradable material, and have a tap density less than  $0.4 \text{ g/cm}^3$ . The "aerodynamically light" particles generally have a mean diameter between  $5 \text{ }\mu\text{m}$  and  $30 \text{ }\mu\text{m}$ . The tap density less than  $0.4 \text{ g/cm}^3$  and mean diameter between  $5 \text{ }\mu\text{m}$  and  $30 \text{ }\mu\text{m}$ , are designed to yield particles with an aerodynamic diameter between approximately one and five microns, preferably between approximately one and three microns. The particles may be formed of biodegradable materials such as biodegradable polymers, proteins, or other water soluble or non-water soluble materials. Particles can also be formed of water-soluble excipients, such as trehalose or lactose, or proteins, such as the proteins to be delivered. In one embodiment, the particles include only a therapeutic or diagnostic agent to be delivered to a patient in a complex with another charged molecule. In a second embodiment, the particles include only the agent and a surfactant. In a third embodiment, particles include surfactant and charged molecules forming a complex, which provides for sustained release.

The particles can be used for enhanced delivery of a therapeutic agent to the airways or the alveolar region of the lung. The particles may be effectively aerosolized for administration to the respiratory tract to permit systemic or local delivery of a wide variety of therapeutic agents. They also optionally may be co-delivered with larger carrier particles, not carrying a therapeutic agent, having, for example, a mean diameter ranging between about  $50 \text{ }\mu\text{m}$  and  $100 \text{ }\mu\text{m}$ . The particles can be used to form a composition that includes the particles and a pharmaceutically

acceptable carrier for administration to a patient, preferably for administration via inhalation.

### Brief Description of the Drawings

Figure 1 is a graph comparing the mass fraction of the initial dose that is released from a dry powder inhaler device, after *in vitro* aerosolization of poly (D,L-lactic-co-glycolic acid) ("PLGA") microspheres made by a double emulsion procedure with and without the incorporation of L- $\alpha$ -phosphatidylcholine dipalmitoyl ("DPPC").

Figure 2 is a graph comparing the mass fraction of the aerosolized dose that is deposited in different stages of a cascade impactor after *in vitro* aerosolization of PLGA microspheres made by a double emulsion procedure with and without the incorporation of DPPC.

Figure 3 is a graph showing the aerosolization behavior of PLGA microspheres made by spray drying with and without the incorporation of DPPC showing the mass-fraction of the initial dose that is released from the dry powder inhaler device after *in vitro* aerosolization.

Figure 4 is a graph comparing the *in vitro* aerosolization behaviors of PLA and PLGA microspheres made by spray drying with and without the incorporation of DPPC showing the mass-fraction of the aerosolized dose that is deposited in stages of a cascade impactor corresponding to the "respirable-fraction".

Figure 5 is a graph comparing the plasma concentration of insulin (ng/ml) per unit time (hrs).

Figure 6 is a graph comparing the release of albuterol (%) over time (hrs).

Figure 7 is a graph comparing the *in vitro* release of albuterol (%) over time (hrs) for compositions with varying ratios of DPPC, albumin, lactose and albuterol.

Figure 8 is a graph comparing the airway resistance change (cm H<sub>2</sub>O/ml/sec.) per unit time (hrs).



### Detailed Description of the Invention

Particles incorporating a surfactant and/or a hydrophilic or hydrophobic complex of a positively or negatively charged therapeutic or diagnostic agent and a charged molecule of opposite charge for delivery to the pulmonary system, and methods for their synthesis and administration are provided. The particles can, but need not include a therapeutic or diagnostic agent. In one embodiment, the particles include either only a therapeutic or diagnostic agent for delivery to a patient. In a second embodiment, the particles include a therapeutic or diagnostic the agent and a surfactant.

The particles have a tap density less than  $0.4 \text{ g/cm}^3$  and a mean diameter between  $5 \text{ }\mu\text{m}$  and  $30 \text{ }\mu\text{m}$ , which in combination yield an aerodynamic diameter of between one and five microns, preferably between one and three microns. The aerodynamic diameter is calculated to provide for maximum deposition within the lungs, previously achieved by the use of very small particles of less than five microns in diameter, preferably between one and three microns, which are then subject to phagocytosis. Selection of particles which have a larger diameter, but which are sufficiently light (hence the characterization "aerodynamically light"), results in an equivalent delivery to the lungs, but the larger size particles are not phagocytosed. Improved delivery can be obtained by using particles with a rough or uneven surface relative to those with a smooth surface. The presence of a surfactant minimizes aggregation of the particles. The presence of a complex of the therapeutic agent with a molecule of opposite charge provides for sustained release of the agent.

The particles can be used for controlled systemic or local delivery of therapeutic or diagnostic agents to the respiratory tract via aerosolization. Administration of the particles to the lung by aerosolization permits deep lung delivery of relatively large diameter therapeutic aerosols, for example, greater than  $5 \text{ }\mu\text{m}$  in mean diameter. The particles can be fabricated with a rough surface texture to reduce particle agglomeration and improve flowability of the powder. The

particles have improved aerosolization properties. The particle can be fabricated with features which enhance aerosolization via dry powder inhaler devices, and lead to lower deposition in the mouth, throat and inhaler device.

- 5           The particles can be used to form a composition that includes the particles and a pharmaceutically acceptable carrier for administration to a patient, preferably for administration via inhalation. Suitable carriers include those typically used for inhalation therapy. Those of skill in the art can readily determine an appropriate pharmaceutically acceptable  
10 carrier for use in administering particles via inhalation.

#### **Particle Materials**

- The particles can be prepared entirely from a therapeutic or diagnostic agent, or from a combination of the agent and a surfactant. The particles preferably are biodegradable and biocompatible, and  
15 optionally are capable of biodegrading at a controlled rate for delivery of a therapeutic or diagnostic agent. The particles can be made of a variety of materials. Both inorganic and organic materials can be used. For example, ceramics may be used. Polymeric and non-polymeric materials, such as fatty acids, may be used to form aerodynamically light particles.  
20 Other suitable materials include, but are not limited to, gelatin, polyethylene glycol, trehalose, and dextran. Particles with degradation and release times ranging from seconds to months can be designed and fabricated, based on factors such as the particle material. Different properties of the particle which can contribute to the aerodynamic  
25 lightness include the composition forming the particle, and the presence of irregular surface structure, or pores or cavities within the particle.

#### *Polymeric Particles*

- Polymeric particles may be formed from any biocompatible, and preferably biodegradable polymer, copolymer, or blend. Preferred  
30 polymers are those which are capable of forming aerodynamically light particles having a tap density less than about 0.4 g/cm<sup>3</sup>, a mean diameter between 5 μm and 30 μm and an aerodynamic diameter between

approximately one and five microns, preferably between one and three microns. The polymers may be tailored to optimize different characteristics of the particle including: i) interactions between the agent to be delivered and the polymer to provide stabilization of the agent and retention of activity upon delivery; ii) rate of polymer degradation and, thereby, rate of drug release profiles; iii) surface characteristics and targeting capabilities via chemical modification; and iv) particle porosity.

Surface eroding polymers such as polyanhydrides may be used to form the particles. For example, polyanhydrides such as poly[(*p*-carboxyphenoxy)-hexane anhydride] (PCPH) may be used. Biodegradable polyanhydrides are described in U.S. Patent No. 4,857,311.

In another embodiment, bulk eroding polymers such as those based on polyesters including poly(hydroxy acids) can be used. For example, polyglycolic acid (PGA), polylactic acid (PLA), or copolymers thereof may be used to form the particles. The polyester may also have a charged or functionalizable group, such as an amino acid. In a preferred embodiment, particles with controlled release properties can be formed of poly(D,L-lactic acid) and/or poly(D,L-lactic-co-glycolic acid) ("PLGA") which incorporate a surfactant such as DPPC.

Other polymers include polyamides, polycarbonates, polyalkylenes such as polyethylene, polypropylene, poly(ethylene glycol), poly(ethylene oxide), poly(ethylene terephthalate), poly vinyl compounds such as polyvinyl alcohols, polyvinyl ethers, and polyvinyl esters, polymers of acrylic and methacrylic acids, celluloses and other polysaccharides, and peptides or proteins, or copolymers or blends thereof. Polymers may be selected with or modified to have the appropriate stability and degradation rates *in vivo* for different controlled drug delivery applications.

In one embodiment, aerodynamically light particles are formed from functionalized polyester graft copolymers, as described in Hrkach *et al.*, *Macromolecules*, 28:4736-4739 (1995); and Hrkach *et al.*, "Poly(L-Lactic acid-co-amino acid) Graft Copolymers: A Class of Functional Biodegradable Biomaterials" in *Hydrogels and Biodegradable Polymers*

*for Bioapplications*, ACS Symposium Series No. 627, Raphael M. Ottenbrite *et al.*, Eds., American Chemical Society, Chapter 8, pp. 93-101, 1996.

Materials other than biodegradable polymers may be used to form the particles. Suitable materials include various non-biodegradable polymers and various excipients. The particles also may be formed of a therapeutic or diagnostic agent and surfactant alone. In one embodiment, the particles may be formed of the surfactant and include a therapeutic or diagnostic agent, to improve aerosolization efficiency due to reduced particle surface interactions, and to potentially reduce loss of the agent due to phagocytosis by alveolar macrophages.

#### *Excipients*

In addition to a therapeutic or diagnostic agent (or possibly other desired molecules for delivery), the particles can include, and preferably, do include, one or more of the following excipients; a sugar, such as lactose, a protein, such as albumin, and/or a surfactant.

#### *Complex Forming Materials*

If the agent to be delivered is negatively charged (such as insulin), protamine or other positively charged molecules can be added to provide a lipophilic complex which results in the sustained release of the negatively charged agent. Negatively charged molecules can be used to render insoluble positively charged agents.

#### *Surfactants*

Surfactants which can be incorporated into particles to improve their aerosolization properties include phosphoglycerides. Exemplary phosphoglycerides include phosphatidylcholines, such as the naturally occurring surfactant, L- $\alpha$ -phosphatidylcholine dipalmitoyl ("DPPC"). The surfactants advantageously improve surface properties by, for example, reducing particle-particle interactions, and can render the surface of the particles less adhesive. The use of surfactants endogenous to the lung may avoid the need for the use of non-physiologic surfactants.

As used herein, the term "surfactant" refers to any agent which preferentially absorbs to an interface between two immiscible phases, such as the interface between water and an organic polymer solution, a water/air interface or organic solvent/air interface. Surfactants generally possess a hydrophilic moiety and a lipophilic moiety, such that, upon absorbing to microparticles, they tend to present moieties to the external environment that do not attract similarly-coated particles, thus reducing particle agglomeration. Surfactants may also promote absorption of a therapeutic or diagnostic agent and increase bioavailability of the agent.

As used herein, a particle "incorporating a surfactant" refers to a particle with a surfactant on at least the surface of the particle. The surfactant may be incorporated throughout the particle and on the surface during particle formation, or may be coated on the particle after particle formation. The surfactant can be coated on the particle surface by adsorption, ionic or covalent attachment, or physically "entrapped" by the surrounding matrix. The surfactant can be, for example, incorporated into controlled release particles, such as polymeric microspheres.

Providing a surfactant on the surfaces of the particles can reduce the tendency of the particles to agglomerate due to interactions such as electrostatic interactions, Van der Waals forces, and capillary action. The presence of the surfactant on the particle surface can provide increased surface rugosity (roughness), thereby improving aerosolization by reducing the surface area available for intimate particle-particle interaction. The use of a surfactant which is a natural material of the lung can potentially reduce opsonization (and thereby reducing phagocytosis by alveolar macrophages), thus providing a longer-lived controlled release particle in the lung.

Surfactants known in the art can be used including any naturally occurring surfactant. Other exemplary surfactants include diphosphatidyl glycerol (DPPG); hexadecanol; fatty alcohols such as polyethylene glycol (PEG); polyoxyethylene-9-lauryl ether; a surface active fatty acid, such as palmitic acid or oleic acid; sorbitan trioleate (Span 85); glycocholate;

surfactin; a poloxomer; a sorbitan fatty acid ester such as sorbitan trioleate; tyloxapol and a phospholipid.

#### *Materials Enhancing Sustained Release*

If the molecules are hydrophilic and tend to solubilize readily in an aqueous environment, another method for achieving sustained release is to use cholesterol or very high surfactant concentration. This complexation methodology also applies to particles that are not aerodynamically light.

#### **Formation of Particles**

##### *Formation of Polymeric Particles*

Polymeric particles may be prepared using single and double emulsion solvent evaporation, spray drying, solvent extraction, solvent evaporation, phase separation, simple and complex coacervation, interfacial polymerization, and other methods well known to those of ordinary skill in the art. Particles may be made using methods for making microspheres or microcapsules known in the art, provided that the conditions are optimized for forming particles with the desired aerodynamic diameter, or additional steps are performed to select particles with the density and diameter sufficient to provide the particles with an aerodynamic diameter between one and five microns, preferably between one and three microns.

Methods developed for making microspheres for delivery of encapsulated agents are described in the literature, for example, as described in Doubrow, M., Ed., "Microcapsules and Nanoparticles in Medicine and Pharmacy," CRC Press, Boca Raton, 1992. Methods also are described in Mathiowitz and Langer, *J. Controlled Release* 5, 13-22 (1987); Mathiowitz *et al.*, *Reactive Polymers* 6, 275-283 (1987); and Mathiowitz *et al.*, *J. Appl. Polymer Sci.* 35, 755-774 (1988). The selection of the method depends on the polymer selection, the size, external morphology, and crystallinity that is desired, as described, for example, by Mathiowitz *et al.*, *Scanning Microscopy* 4: 329-340 (1990); Mathiowitz *et al.*, *J. Appl. Polymer Sci.* 45, 125-134 (1992); and Benita *et al.*, *J. Pharm. Sci.* 73, 1721-1724 (1984).

In solvent evaporation, described for example, in Mathiowitz *et al.*, (1990), Benita; and U.S. Patent No. 4,272,398 to Jaffe, the polymer is dissolved in a volatile organic solvent, such as methylene chloride. Several different polymer concentrations can be used, for example, 5 between 0.05 and 1.0 g/ml. The therapeutic or diagnostic agent, either in soluble form or dispersed as fine particles, is added to the polymer solution, and the mixture is suspended in an aqueous phase that contains a surface active agent such as poly(vinyl alcohol). The aqueous phase may be, for example, a concentration of 1% poly(vinyl alcohol) w/v in 10 distilled water. The resulting emulsion is stirred until most of the organic solvent evaporates, leaving solid microspheres, which may be washed with water and dried overnight in a lyophilizer. Microspheres with different sizes (between 1 and 1000 microns) and morphologies can be obtained by this method.

15 Solvent removal was primarily designed for use with less stable polymers, such as the polyanhydrides. In this method, the agent is dispersed or dissolved in a solution of a selected polymer in a volatile organic solvent like methylene chloride. The mixture is then suspended in oil, such as silicon oil, by stirring, to form an emulsion. Within 24 20 hours, the solvent diffuses into the oil phase and the emulsion droplets harden into solid polymer microspheres. Unlike the hot-melt microencapsulation method described for example in Mathiowitz *et al.*, *Reactive Polymers*, 6:275 (1987), this method can be used to make microspheres from polymers with high melting points and a wide range of 25 molecular weights. Microspheres having a diameter for example between one and 300 microns can be obtained with this procedure.

With some polymeric systems, polymeric particles prepared using a single or double emulsion technique vary in size depending on the size of the droplets. If droplets in water-in-oil emulsions are not of a suitably 30 small size to form particles with the desired size range, smaller droplets can be prepared, for example, by sonication or homogenation of the emulsion, or by the addition of surfactants.

If the particles prepared by any of the above methods have a size range outside of the desired range, particles can be sized, for example, using a sieve, and further separated according to density using techniques known to those of skill in the art.

- 5           The polymeric particles are preferably prepared by spray drying. Prior methods of spray drying, such as that disclosed in PCT WO 96/09814 by Sutton and Johnson, disclose the preparation of smooth, spherical microparticles of a water-soluble material with at least 90% of the particles possessing a mean size between 1 and 10  $\mu\text{m}$ . The method  
10       disclosed herein provides rough (non-smooth), non-spherical microparticles that include a water-soluble material combined with a water-insoluble material. At least 90% of the particles possess a mean size between 5 and 30  $\mu\text{m}$ , and a low mass or tap density (less than 0.4 g/cc).
- 15           The particles can incorporate various complexes of therapeutic or diagnostic agents to be delivered with molecules of an opposite charge, or can include substances such as lipids which allow for the sustained release of small and large molecules. Addition of these complexes or substances  
20       is applicable to particles of any size and shape, and is especially useful for altering the rate of release of therapeutic agents from inhaled particles.

#### **Aerodynamically Light Particles**

- Aerodynamically light particles, having a tap density less than about 0.4 g/cm<sup>3</sup> and an aerodynamic diameter between one and five microns, preferably between one and three microns, may be fabricated  
25       using the methods disclosed herein.

#### *Aerodynamically Light Particle Size*

- The mass mean diameter of the particles can be measured using a Coulter Multisizer II (Coulter Electronics, Luton, Beds, England). The aerodynamically light particles in one preferred embodiment are at least  
30       about 5 microns in diameter. The diameter of particles in a sample will range depending upon factors such as particle composition and methods of



synthesis. The distribution of size of particles in a sample can be selected to permit optimal deposition within targeted sites within the respiratory tract.

5 The aerodynamically light particles may be fabricated or separated, for example by filtration or centrifugation, to provide a particle sample with a preselected size distribution. For example, greater than 30%, 50%, 70%, or 80% of the particles in a sample can have a diameter within a selected range of at least 5  $\mu\text{m}$ . The selected range within which a certain percentage of the particles must fall may be for example, 10 between about 5 and 30  $\mu\text{m}$ , or optionally between 5 and 15  $\mu\text{m}$ . In one preferred embodiment, at least a portion of the particles have a diameter between about 9 and 11  $\mu\text{m}$ . Optionally, the particle sample also can be fabricated wherein at least 90%, or optionally 95% or 99%, have a diameter within the selected range. The presence of the higher proportion 15 of the aerodynamically light, larger diameter (at least about 5  $\mu\text{m}$ ) particles in the particle sample enhances the delivery of therapeutic or diagnostic agents incorporated therein to the deep lung.

In one embodiment, in the particle sample, the interquartile range may be 2  $\mu\text{m}$ , with a mean diameter for example, between about 7.5 and 20 13.5  $\mu\text{m}$ . Thus, for example, between at least 30% and 40% of the particles may have diameters within the selected range. Preferably, the said percentages of particles have diameters within a 1  $\mu\text{m}$  range, for example, between 6.0 and 7.0  $\mu\text{m}$ , 10.0 and 11.0  $\mu\text{m}$  or 13.0 and 14.0  $\mu\text{m}$ .

25 The aerodynamically light particles, optionally incorporating a therapeutic or diagnostic agent, with a tap density less than about 0.4  $\text{g}/\text{cm}^3$ , mean diameters of at least about 5  $\mu\text{m}$ , and an aerodynamic diameter of between one and five microns, preferably between one and three microns, are more capable of escaping inertial and gravitational 30 deposition in the oropharyngeal region, and are targeted to the airways or the deep lung. The use of larger particles (mean diameter at least about 5  $\mu\text{m}$ ) is advantageous since they are able to aerosolize more efficiently

than smaller, denser aerosol particles such as those currently used for inhalation therapies.

In comparison to smaller, relatively denser particles, the larger (at least about 5  $\mu\text{m}$ ) aerodynamically light particles also can potentially more successfully avoid phagocytic engulfment by alveolar macrophages and clearance from the lungs, due to size exclusion of the particles from the phagocytes' cytosolic space. Phagocytosis of particles by alveolar macrophages diminishes precipitously as particle diameter increases beyond 3  $\mu\text{m}$ . Kawaguchi, H. *et al.*, *Biomaterials* 7: 61-66 (1986); Krenis, L.J. and Strauss, B., *Proc. Soc. Exp. Med.*, 107:748-750 (1961); and Rudt, S. and Muller, R.H., *J. Contr. Rel.*, 22: 263-272 (1992). For particles of statistically isotropic shape, such as spheres with rough surfaces, the particle envelope volume is approximately equivalent to the volume of cytosolic space required within a macrophage for complete particle phagocytosis.

Aerodynamically light particles thus are capable of a longer term release of an encapsulated agent in the lungs. Following inhalation, aerodynamically light biodegradable particles can deposit in the lungs (due to their relatively low tap density), and subsequently undergo slow degradation and drug release, without the majority of the particles being phagocytosed by alveolar macrophages. The drug can be delivered relatively slowly into the alveolar fluid, and at a controlled rate into the blood stream, minimizing possible toxic responses of exposed cells to an excessively high concentration of the drug. The aerodynamically light particles thus are highly suitable for inhalation therapies, particularly in controlled release applications.

The preferred mean diameter for aerodynamically light particles for inhalation therapy is at least about 5  $\mu\text{m}$ , for example between about 5 and 30  $\mu\text{m}$ . The particles may be fabricated with the appropriate material, surface roughness, diameter and tap density for localized delivery to selected regions of the respiratory tract such as the deep lung or upper airways. For example, higher density or larger particles may be

used for upper airway delivery, or a mixture of different sized particles in a sample, provided with the same or different therapeutic agent may be administered to target different regions of the lung in one administration.

*Density and Deposition of Aerodynamically Light Particles*

5 As used herein, the phrase "aerodynamically light particles" refers to particles having a tap density less than about 0.4 g/cm<sup>3</sup>. The tap density of particles of a dry powder may be obtained using a GeoPyc™ (Micrometrics Instrument Corp., Norcross, GA 30093). Tap density is a standard measure of the envelope mass density. The envelope mass  
10 density of an isotropic particle is defined as the mass of the particle divided by the minimum sphere envelope volume within which it can be enclosed. Features which can contribute to low tap density include irregular surface texture and porous structure.

Inertial impaction and gravitational settling of aerosols are  
15 predominant deposition mechanisms in the airways and acini of the lungs during normal breathing conditions. Edwards, D.A., *J. Aerosol Sci.*, 26: 293-317 (1995). The importance of both deposition mechanisms increases in proportion to the mass of aerosols and not to particle (or envelope) volume. Since the site of aerosol deposition in the lungs is determined by  
20 the mass of the aerosol (at least for particles of mean aerodynamic diameter greater than approximately 1 μm), diminishing the tap density by increasing particle surface irregularities and particle porosity permits the delivery of larger particle envelope volumes into the lungs, all other physical parameters being equal.

25 The low tap density particles have a small aerodynamic diameter in comparison to the actual envelope sphere diameter. The aerodynamic diameter,  $d_{\text{acr}}$ , is related to the envelope sphere diameter,  $d$  (Gonda, I., "Physico-chemical principles in aerosol delivery," in *Topics in Pharmaceutical Sciences 1991* (eds. D.J.A. Crommelin and K.K. Midha), pp. 95-117, Stuttgart: Medpharm Scientific Publishers, 1992)),  
30 by the formula:

$$d_{\text{acr}} = d\sqrt{\rho}$$

where the envelope mass  $\rho$  is in units of  $\text{g/cm}^3$ . Maximal deposition of monodisperse aerosol particles in the alveolar region of the human lung ( $\sim 60\%$ ) occurs for an aerodynamic diameter of approximately  $d_{\text{acr}} = 3 \mu\text{m}$ .

- 5 Heyder, J. *et al.*, *J. Aerosol Sci.*, 17: 811-825 (1986). Due to their small envelope mass density, the actual diameter  $d$  of aerodynamically light particles comprising a monodisperse inhaled powder that will exhibit maximum deep-lung deposition is:

10 
$$d = 3/\sqrt{\rho} \mu\text{m} \text{ (where } \rho < 1 \text{ g/cm}^3\text{);}$$

- where  $d$  is always greater than  $3 \mu\text{m}$ . For example, aerodynamically light particles that display an envelope mass density,  $\rho = 0.1 \text{ g/cm}^3$ , will exhibit a maximum deposition for particles having envelope diameters as large as  $9.5 \mu\text{m}$ . The increased particle size diminishes interparticle  
15 adhesion forces. Visser, J., *Powder Technology*, 58:1-10. Thus, large particle size increases efficiency of aerosolization to the deep lung for particles of low envelope mass density, in addition to contributing to lower phagocytic losses.

#### Targeting of Particles

- 20 Targeting molecules can be attached to the particles via reactive functional groups on the particles. For example, targeting molecules can be attached to the amino acid groups of functionalized polyester graft copolymer particles, such as poly(lactic acid-co-lysine) (PLAL-Lys) particles. Targeting molecules permit binding interaction of the particle  
25 with specific receptor sites, such as those within the lungs. The particles can be targeted by attachment of ligands which specifically or non-specifically bind to particular targets. Exemplary targeting molecules include antibodies and fragments thereof including the variable regions, lectins, and hormones or other organic molecules capable of specific  
30 binding, for example, to receptors on the surfaces of the target cells.

### Therapeutic Agents

Any of a variety of therapeutic or prophylactic agents can be incorporated within the particles, or used to prepare particles consisting solely of the agent and surfactant. The particles can be used to locally or  
5 systemically deliver a variety of incorporated agents to an animal. Examples include synthetic inorganic and organic compounds, proteins and peptides, polysaccharides and other sugars, lipids, and DNA and RNA nucleic acid sequences having therapeutic, prophylactic or diagnostic activities. Nucleic acid sequences include genes, antisense  
10 molecules which bind to complementary DNA to inhibit transcription, and ribozymes. The agents to be incorporated can have a variety of biological activities, such as vasoactive agents, neuroactive agents, hormones, anticoagulants, immunomodulating agents, cytotoxic agents, prophylactic agents, antibiotics, antivirals, antisense, antigens, and antibodies. In  
15 some instances, the proteins may be antibodies or antigens which otherwise would have to be administered by injection to elicit an appropriate response. Compounds with a wide range of molecular weight can be encapsulated, for example, between 100 and 500,000 grams or more per mole.

20 Proteins are defined as consisting of 100 amino acid residues or more; peptides are less than 100 amino acid residues. Unless otherwise stated, the term protein refers to both proteins and peptides. Examples include insulin and other hormones. Polysaccharides, such as heparin, can also be administered.

25 The polymeric aerosols are useful as carriers for a variety of inhalation therapies. They can be used to encapsulate small and large drugs, release encapsulated drugs over time periods ranging from hours to months, and withstand extreme conditions during aerosolization or following deposition in the lungs that might otherwise harm the  
30 encapsulated therapeutic.

The particles may include a therapeutic agent for local delivery within the lung, such as agents for the treatment of asthma, emphysema,

or cystic fibrosis, or for systemic treatment. For example, genes for the treatment of diseases such as cystic fibrosis can be administered, as can beta agonists for asthma. Other specific therapeutic agents include, but are not limited to, insulin, calcitonin, leuprolide (or gonadotropin-releasing hormone ("LHRH")), granulocyte colony-stimulating factor ("G-CSF"), parathyroid hormone-related peptide, somatostatin, testosterone, progesterone, estradiol, nicotine, fentanyl, norethisterone, clonidine, scopolomine, salicylate, cromolyn sodium, salmeterol, formeterol, albuterol, and valium.

Those therapeutic agents which are charged, such as most of the proteins, including insulin, can be administered as a complex between the charged therapeutic agent and a molecule of opposite charge. Preferably, the molecule of opposite charge is a charged lipid or an oppositely charged protein.

#### **Diagnostic agents**

Any of a variety of diagnostic agents can be incorporated within the particles, which can locally or systemically deliver the incorporated agents following administration to a patient. Any biocompatible or pharmacologically acceptable gas can be incorporated into the particles or trapped in the pores of the particles using technology known to those skilled in the art. The term gas refers to any compound which is a gas or capable of forming a gas at the temperature at which imaging is being performed. In one embodiment, retention of gas in the particles is improved by forming a gas-impermeable barrier around the particles. Such barriers are well known to those of skill in the art.

Other imaging agents which may be utilized include commercially available agents used in positron emission tomography (PET), computer assisted tomography (CAT), single photon emission computerized tomography, x-ray, fluoroscopy, and magnetic resonance imaging (MRI).

Examples of suitable materials for use as contrast agents in MRI include the gadolinium chelates currently available, such as diethylene

triamine pentacetic acid (DTPA) and gadopentotate dimeglumine, as well as iron, magnesium, manganese, copper and chromium.

Examples of materials useful for CAT and x-rays include iodine based materials for intravenous administration, such as ionic monomers typified by diatrizoate and iothalamate, non-ionic monomers such as iopamidol, isohexol, and ioversol, non-ionic dimers, such as iotrol and iodixanol, and ionic dimers, for example, ioxagalte.

Porous particles can be prepared which can be delivered via pulmonary delivery, and used, for example, for local or systemic delivery of incorporated agents and/or for imaging purposes. Particles incorporating diagnostic agents can be detected using standard techniques available in the art and commercially available equipment.

#### Administration

The particles may be administered alone or in any appropriate pharmaceutically acceptable carrier, such as a liquid, for example saline, or a powder, for administration to the respiratory system. They can be co-delivered with larger carrier particles, not including a therapeutic agent, the latter possessing mass mean diameters for example in the range between 50  $\mu\text{m}$  and 100  $\mu\text{m}$ .

Aerosol dosage, formulations and delivery systems may be selected for a particular therapeutic application, as described, for example, in Gonda, I. "Aerosols for delivery of therapeutic and diagnostic agents to the respiratory tract," in *Critical Reviews in Therapeutic Drug Carrier Systems*, 6:273-313, 1990; and in Moren, "Aerosol dosage forms and formulations," in: *Aerosols in Medicine. Principles, Diagnosis and Therapy*, Moren, et al., Eds, Eisevier, Amsterdam, 1985.

The greater efficiency of aerosolization by the particles disclosed herein relative to particles that do not include a surfactant or a charged complex of a therapeutic agent permits more of a therapeutic agent to be delivered. The use of biodegradable polymers permits controlled release in the lungs and long-time local action or systemic bioavailability.

Denaturation of macromolecular drugs can be minimized during aerosolization since macromolecules can be contained and protected within a polymeric shell. Coencapsulation of peptides with peptidase-inhibitors can minimize peptide enzymatic degradation. Pulmonary delivery advantageously can eliminate the need for injection. For example, the requirement for daily insulin injections can be avoided.

The present invention will be further understood by reference to the following non-limiting examples.

**Example 1: Synthesis of Aerodynamically Light Poly[(p-carboxyphenoxy)-hexane anhydride] ("PCPH") Particles**

Aerodynamically light poly[(p-carboxyphenoxy)-hexane anhydride] ("PCPH") particles were synthesized as follows. 100 mg PCPH (MW ~ 25,000) was dissolved in 3.0 mL methylene chloride. To this clear solution was added 5.0 mL 1% w/v aqueous polyvinyl alcohol (PVA, MW ~ 25,000, 88 mole % hydrolyzed) saturated with methylene chloride, and the mixture was vortexed (Vortex Genie 2, Fisher Scientific) at maximum speed for one minute. The resulting milky-white emulsion was poured into a beaker containing 95 mL 1% PVA and homogenized (Silverson Homogenizers) at 6000 RPM for one minute using a 0.75 inch tip. After homogenization, the mixture was stirred with a magnetic stirring bar and the methylene chloride quickly extracted from the polymer particles by adding 2 mL isopropyl alcohol. The mixture was continued to stir for 35 minutes to allow complete hardening of the microparticles. The hardened particles were collected by centrifugation and washed several times with double distilled water. The particles were freeze dried to obtain a free-flowing powder void of clumps. Yield, 85-90%.

The mean diameter of a typical batch prepared by this protocol is 6.0  $\mu\text{m}$ , however, particles with mean diameters ranging from a few hundred nanometers to several millimeters may be made with only slight modifications. Scanning electron micrograph photos of a typical batch of



PCPH particles showed the particles to be highly porous with irregular surface shape. The particles have a tap density less than 0.4 g/cm<sup>3</sup>.

A surfactant such as DPPC may be incorporated into the polymer solution prior to particle formation, or optionally the particles can be ionically or covalently coated by surfactant on the particle surface after particle formation, or the surfactant may be absorbed onto the particle surface.

#### Example 2: Synthesis of Spray-Dried Particles.

##### *Aerodynamically Light Particles Containing Polymer and Drug Soluble in Common Solvent*

Aerodynamically light 50:50 PLGA particles were prepared by spray drying with testosterone encapsulated within the particles according to the following procedures. 2.0 g poly (D,L-lactic-co-glycolic acid) with a molar ratio of 50:50 (PLGA 50:50, Resomer RG503, B.I. Chemicals, Montvale, NJ) and 0.50 g testosterone (Sigma Chemical Co., St. Louis, MO) are completely dissolved in 100 mL dichloromethane at room temperature. The mixture is subsequently spray-dried through a 0.5 mm nozzle at a flow rate of 5 mL/min using a Buchi laboratory spray-drier (model 190, Buchi, Germany). The flow rate of compressed air is 700 nl. The inlet temperature is set to 30°C and the outlet temperature to 25°C. The aspirator is set to achieve a vacuum of -20 to -25 bar. The yield is 51% and the mean particle size is approximately 5 μm. Larger particle size can be achieved by lowering the inlet compressed air flow rate, as well as by changing other variables. The particles are aerodynamically light, as determined by a tap density less than or equal to 0.4 g/cm<sup>3</sup> and an aerodynamic diameter between one and five microns. Porosity and surface roughness can be increased by varying the inlet and outlet temperatures, among other factors.

##### *Aerodynamically Light Particles Containing Polymer and Drug in Different Solvents*

Aerodynamically light PLA particles with a model hydrophilic drug (dextran) were prepared by spray drying using the following

procedure. 2.0 mL of an aqueous 10% w/v FITC-dextran (MW 70,000, Sigma Chemical Co.) solution was emulsified into 100 mL of a 2% w/v solution of poly (D,L-lactic-acid) (PLA, Resomer R206, B.I. Chemicals) in dichloromethane by probe sonication (Sonics & Materials, Model VC-5 250 sonicator, Danbury, CT). The emulsion is subsequently spray-dried at a flow rate of 5 mL/min with an air flow rate of 700 nl/h (inlet temperature = 30°C, outlet temperature = 21°C, -20 mbar vacuum). The yield is 56%.

*Aerodynamically Light Protein Particles*

10 Aerodynamically light lysozyme particles were prepared by spray drying using the following procedure. 4.75 g lysozyme (Sigma) was dissolved in 95 mL double distilled water (5% w/v solution) and spray-dried using a 0.5 mm nozzle and a Buchi laboratory spray-drier. The flow rate of compressed air was 725 nl/h. The flow rate of the lysozyme 15 solution was set such that, at a set inlet temperature of between 97 and 100°C, the outlet temperature is between 55 and 57°C. The aspirator was set to achieve a vacuum of -30 mbar. The enzymatic activity of lysozyme was found to be unaffected by this process and the yield of the aerodynamically light particles was 66%.

20 *Aerodynamically Light High-Molecular Weight Water-Soluble Particles*

Aerodynamically light dextran particles were prepared by spray drying using the following procedure. 6.04 g DEAE dextran (Sigma) was dissolved in 242 mL double distilled water (2.5% w/v solution) and 25 spray-dried using a 0.5 mm nozzle and a Buchi laboratory spray-drier. The flow rate of compressed air was 750 nl/h. The flow rate of the DEAE-dextran solution was set such that, at a set inlet temperature of 155°C, the outlet temperature was 80°C. The aspirator was set to achieve a vacuum of -20 mbar. The yield of the aerodynamically light 30 particles was 66%.

*Aerodynamically Light Low-Molecular Weight Water-Soluble Particles*

Aerodynamically light trehalose particles were prepared by spray drying using the following procedure. 4.9 g trehalose (Sigma) was dissolved in 192 mL double distilled water (2.5% w/v solution) and spray-dried using a 0.5 mm nozzle and a Buchi laboratory spray-drier.

- 5 The flow rate of compressed air 650 nl/h. The flow rate of the trehalose solution was set such that, at a set inlet temperature of 100°C, the outlet temperature was 60°C. The aspirator was set to achieve a vacuum of -30 mbar. The yield of the aerodynamically light particles was 36%.

*Aerodynamically Light Low-Molecular Weight Water-Soluble Particles*

10

Polyethylene glycol (PEG) is a water-soluble macromolecule, however, it cannot be spray dried from an aqueous solution since it melts at room temperatures below that needed to evaporate water. As a result, PEG was spray-dried at low temperatures from a solution in

- 15 dichloromethane, a low-boiling organic solvent. Aerodynamically light PEG particles were prepared by spray drying using the following procedure. 5.0 g PEG (MW between 15,000 and 20,000, Sigma) was dissolved in 100 mL double distilled water (5.0% w/v solution) and spray-dried using a 0.5 mm nozzle and a Buchi laboratory spray-drier.

- 20 The flow rate of compressed air 750 nl/h. The flow rate of the PEG solution was set such that, at a set inlet temperature of 45°C, the outlet temperature was between 34 and 35°C. The aspirator was set to achieve a vacuum of -22 mbar. The yield of the aerodynamically light particles (tap density less than 0.4 g/cm<sup>3</sup>) was 67%.

- 25 A surfactant such as DPPC may be incorporated into the polymer solution prior to particle formation, or optionally the particles can be ionically or covalently coated by surfactant on the particle surface after particle formation, or the surfactant may be absorbed onto the particle surface.

## Materials and Methods

The following materials and methods were used in Examples 3 and

4.

### Materials

5       The polymers: poly(D,L-lactic-co-glycolic acid) (PLGA) with a molar ratio of 50:50 and reported molecular weights of 100,000 Daltons (PLGA RG506) and 34,000 Daltons (PLGA RG503), and poly(D,L-lactic acid) with a reported molecular weight of 100,000 Daltons (PLA R206) were obtained from Boehringer Ingelheim (distributed by B.I. Chemicals, 10 Montvale, NJ). Fluorescently labelled FITC-Dextran with an average molecular weight of 19,000, and L, $\alpha$ -phosphatidylcholine dipalmitoyl (DPPC) were purchased from Sigma Chemical Company, St. Louis, MO.

### Microsphere Preparation: Double Emulsion

A double-emulsion solvent-evaporation procedure (Cohen, S., *et al.*, *Pharm. Res.*, 8(6): 713-720 (1991); and Tabata, Y., *et al.*, *Pharm. Res.*, 10(4): 487-496 (1993)), was modified to prepare microspheres for aerosolization. Briefly, 300  $\mu$ l of an aqueous FITC-Dextran solution (50 mg/ml) was emulsified on ice into a 4.0 ml polymer solution in methylene chloride (200 mg polymer) by sonication at output 3 (Model VC-250, 20 Sonics & Materials Inc., Danbury, CT) using a microtip for 5-10 s to form the inner-emulsion. The first emulsion was poured into 100 ml 1.0 % aqueous PVA solution and homogenized (Model LD4 Homogenizer, Silverson Machines Ltd, England) at 6000 RPM using a 5/8" tip for 1 min to form the double emulsion. The microspheres were continuously 25 stirred for 3 hours to allow hardening, collected by centrifugation, washed several times with double-distilled water, and freeze-dried into a freely flowing powder. Microspheres containing DPPC were prepared by dissolving DPPC in the polymer solution at a concentration of 3 mg/ml prior to the initial emulsification.

### 30       Microsphere Preparation: Spray Drying

The model hydrophilic drug, dextran labeled with fluorescein isothiocyanate (FITC-Dextran), was encapsulated into PLA or PLGA by a

novel emulsion/spray method. For example, 2.0 ml of an aqueous 10% w/v FITC-Dextran (MW=70,000, Sigma Chemical Co.) solution was emulsified into 100 ml of a 2 % w/v solution of PLA in dichloromethane by probe sonication. The emulsion was subsequently spray-dried using a  
5 Büchi Mini Spray Drier (Model 190, Büchi Instruments, Germany) at a flow rate of 5 ml/min with an inlet air flow rate of 700 nl/h, inlet temperature of 30°C, outlet temperature of 21°C, and vacuum of - 20 mbar. When DPPC was incorporated it was dissolved in the polymer solution at a concentration of 2 mg/ml prior to emulsification and spray  
10 drying.

#### Microsphere Size Distribution Analysis

Microsphere size distributions were determined using a Coulter Multisizer II (Coulter Electronics Limited, Luton, Beds, England). Approximately 10 drops Coulter type IA non-ionic dispersant were added,  
15 followed by 2 mL isoton II solution (Coulter), to 5-10 mg microspheres, and the spheres were dispersed by brief vortex mixing. This suspension was added to 50 mL isoton II solution until the coincidence of particles was between 5 and 8 %. Greater than 500,000 particles were counted for each batch of spheres.

#### Drug Distribution by Confocal Microscopy

For confocal microscopy, a few milligrams of microspheres containing FITC-Dextran as the drug were suspended in glycerin by brief probe sonication (Vibra-cell Model VC-250 Sonicator, 1/8" microtip probe, Sonics & Materials Inc., Danbury, CT) at output 4 (50W). A  
25 drop of the suspension was placed onto a glass slide and a glass cover slip was applied and held in place with finger nail polish. The suspension was allowed to settle for one hour before being viewed by confocal microscopy (Bio-Rad MRC-600 Confocal, Axioplan microscope).

#### Microsphere Morphology by Scanning Electron Microscopy (SEM)

30 Microsphere morphology was observed by scanning electron microscopy (SEM) using a Stereoscan 250 MK3 microscope from Cambridge Instruments (Cambridge, MA) at 15 kV. Microspheres were

freeze-dried, mounted on metal stubs with double-sided tape, and coated with gold prior to observation.

#### Microsphere Density Analysis

Microsphere bulk density was estimated by tap density  
5 measurements and confirmed by mercury intrusion analysis at Porous Materials, Inc. (Ithaca, NY).

#### Determination of Amount FITC-Dextran and DPPC Encapsulated

The amount of model drug, FITC-Dextran, encapsulated into microspheres was determined by dissolving 10.0 mg microspheres in 3.0  
10 ml 0.8 N NaOH overnight at 37°C, filtering with a 0.45  $\mu$ m filter (Millipore), and measuring the fluorescence relative to a standard curve (494 nm excitation and 525 nm emission) using a fluorimeter. The drug loading was determined by dividing the amount of FITC-Dextran encapsulated by the theoretical amount if it all were encapsulated. The  
15 amount of surfactant, DPPC, encapsulated into microspheres was determined by dissolving 10.0 mg of microspheres in chloroform and using the Stewart Assay (New, R.R.C., "Characterization of Liposomes," in *Liposomes: A Practical Approach*, R. New, Editor, IRL Press, New York, 105-161 (1990)).

#### In Vitro Aerosolization and Inertial Deposition Behavior

The *in vitro* microparticle aerodynamic characteristics were studied using an Andersen Mark I Cascade Impactor (Andersen Samplers, Atlanta, GA) at an air flow rate of 28.3 l/min. The metal impaction plates were coated with a thin film of Tween 80 minimize particle  
25 bouncing Turner, J. and S. Hering, *J. Aerosol Sci.*, 18: 215-224 (1987). Gelatin capsules (Eli Lilly) were charged with 20 mg of microparticles and loaded into a Spinhaler® inhalation device (Fisons, Bedford, MA). The aerosolization experiments were done in triplicate. In each experiment, 10 inhalers were discharged for 30 seconds into the impactor.  
30 A 60-second interval was observed between every two consecutive aerosolizations. Fractions of microspheres deposited on each of nine stages, corresponding to stages 0 to 7, and the filter (F) of the impactor,

were collected in volumetric flasks by carefully washing the plates with NaOH solution (0.8 N) in order to provide degradation of the polymer and complete dissolution of the fluorescent material. After 12 hours of incubation at 37°C, the solutions were filtered with a 0.45  $\mu$ m filter and the amount of fluorescent material in each stage was measured at 494 nm (excitation) and 525 nm (emission) using a fluorimeter. Respirable fraction of the delivered dose was calculated according to the fluorescence measurements as percentages of the total fluorescence (i.e., that amount collected in stages 0 to Filter) compared with that collected in stages 2 to Filter of the Impactor.

*In Vivo* Particle Distribution Following Aerosolization in Rats

Male Sprague Dawley rats (between 150 and 200 g) were anesthetized using a mixture of ketamine (90 mg/kg) and xylazine (10 mg/kg). The anesthetized rat was placed ventral side up on a surgical table provided with a temperature controlled pad to maintain physiological temperature. The animal was cannulated above the carina with an endotracheal tube connected to a Harvard ventilator (Rodent Ventilator Model 683, South Natick, MA). The animal was force ventilated for 20 minutes at 300 ml/min. 50 mg of microspheres made with or without DPPC were introduced into the endotracheal tube. Following the period of forced ventilation, the animal was sacrificed and the lungs and trachea were separately washed using bronchialalveolar lavage as follows: a tracheal cannula was inserted, tied into place, and the airways were washed with 10 ml aliquots of phenol red-free Hanks balanced salt solution (Gibco, Grand Island, NY) without  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  (HBSS). The lavage procedure was repeated until a total volume of 30 ml was collected. The lavage fluid was centrifuged (400 g) and the pellets collected and resuspended in 2 ml HBSS. 100  $\mu$ l was removed for particle counting using a hemacytometer. The remaining solution was mixed with 10 ml of 0.4 N NaOH. After incubation at 37°C for 12 hours, the fluorescence of each solution was measured (wavelengths of 494 nm excitation, 525 nm emission) using a fluorimeter.

**Example 3: Fabrication of PLGA microspheres by a Double Emulsion Process Which Encapsulate a Model High-Molecular-Weight Drug, FITC-Dextran.**

5 Scanning electron microscopy "SEM" photographs showing surface morphology of microspheres (MS) made by the double emulsion process with and without the lung surfactant, DPPC were obtained. By SEM, the microspheres made with and without DPPC by the double emulsion process had very similar surface characteristics and size distribution, as confirmed by size distribution measurements, shown below in Table 1.

10 The efficient entrapment of DPPC within microspheres (83% of theoretical  $\pm$  11% standard deviation, n=6) was confirmed by dissolving an aliquot of MS in chloroform and detecting the DPPC concentration in solution by the Stewart Assay, as shown in Table 1. Particles made by double emulsion with DPPC are easily resuspended in aqueous solution  
15 after lyophilization and are lump-free when dry as determined by light microscopy. Particles made by the double emulsion process without DPPC resuspend easily, however, they appear somewhat agglomerated when dry by light microscopy.



**Table 1. Characteristics of Microparticles used for *In Vitro* and *In Vivo* Aerosolization<sup>a</sup>**

Sample	Mass-Mean (True) Diameter, ( $\mu\text{m}$ )	DPPC Load ( $\mu\text{g}/\text{mg}$ spheres)	DPPC Loading Efficiency, (%)	FITC-Dextran (Model Drug) Loading Efficiency, (%)
MS without DPPC	$8.5 \pm 0.76$	0	N/A	95.8
MS with DPPC	$8.2 \pm 0.18$	$45 \pm 6$	$83 \pm 11$	82.4

<sup>a</sup> Values are given  $\pm$  standard deviation.

Confocal microscopy was used to evaluate the distribution of the model drug, FITC-Dextran ( $M_w$  19,000), throughout microspheres made without DPPC and with DPPC. In each case, the drug is evenly dispersed throughout the polymer matrix, which can lead to prolonged delivery of macromolecules after placement in an aqueous environment.

The density of the microspheres as determined by mercury intrusion analysis is shown in Table 2 (and confirmed by tap density measurements).

**Table 2. Comparison of Porous Microparticles with Bulk (PLGA 50:50) Polymer**

Sample	Density, $\rho_{\text{MS}}$ (g/cc)	Respirable Size Range, $d_{\text{resp}}$ ( $\mu\text{m}$ )
Bulk PLGA	1.35	0.69 - 4.05
MS without DPPC	$0.37 \pm 0.03$	1.3 - 7.7
MS with DPPC	$0.30 \pm 0.06$	1.46 - 8.58

Using the concept of aerodynamic diameter (Gonda, I., in *Topics in Pharmaceutical Sciences 1991*, D. Crommelin and K. Midha, Editors, Stuttgart: Medpharm Scientific Publishers, pp. 95-117 (1992)), it is possible to determine the size range of the microspheres which are

theoretically respirable given their mass density,  $\rho_{MS}$ . Specifically, it can be shown below in Equation 2 that:

$$\frac{0.8}{\sqrt{\rho_{MS}}} \leq d_{resp} \leq \frac{4.7}{\sqrt{\rho_{MS}}} \quad (2)$$

5

where  $d_{resp}$  corresponds to the diameter of particles (in  $\mu m$ ) theoretically able to enter and remain in the airways without inertial or gravitational deposition (particles smaller than this range are exhaled), and where  $\rho_{MS}$  is in units of g/cc. The theoretical respirable size range of the microspheres also is shown in Table 2. The optimal size range (*i.e.*,  $d_{resp}$ ) for a non-porous PLGA 50:50 microsphere is 0.69-4.05  $\mu m$  (Table 2). The optimal respirable size range for microspheres without DPPC is 1.3-7.7  $\mu m$  and, for microspheres with DPPC, 1.46 - 8.58  $\mu m$  (Table 2). The upper limit on size of respirable particles is increased from 4.05 to greater than 8.5  $\mu m$  when DPPC is used in the PLGA microsphere preparation. Therefore, the use of low density DPPC microspheres allows the use of larger particles for aerosolization, which may have advantages for drug delivery, such as less particle-particle interaction due to decreased surface area to volume ratio, and lower susceptibility to phagocytosis by alveolar macrophages. In addition, a primary effect of DPPC is to render the particles less adhesive and therefore allow improved aerosolization, as demonstrated below.

Figures 1 and 2 show the results of an *in vitro* aerosolization of the PLGA microspheres made by a double emulsion process with and without DPPC. The microspheres were aerosolized as a dry powder released from a Spinhaler® dry powder inhaler (DPI). Figure 1 illustrates the mass-fraction of the initial dose that is released from the dry powder inhaler device (DPI Efficiency) using an Andersen Mark I Cascade Impactor. DPI efficiencies approaching 80% were obtained with microspheres made with and without DPPC. Although the DPI

30

efficiencies for the two batches were nearly the same, a great difference can be seen between microspheres made with and without DPPC when their deposition within the cascade impactor is observed (Figure 2).

Figure 2 shows the mass fraction of aerosolized particles that is deposited in stages 2 through Filter (2-Filter) of the Andersen cascade impactor, considered the stages corresponding to the respirable fraction of the microspheres. Stages 0 and 1 correspond roughly to the mouth and throat, and to the upper airways of the lung, respectively. Stages 2-F correspond to successively deeper fractions of the lung. It can be seen that a much greater percentage of microspheres make it to the latter stages of the impactor (considered deeper portions of the lungs) when DPPC is used in their preparation. Overall, greater than 35% ( $37.0 \pm 2.1$ ) of aerosolized particles made with DPPC are considered respirable compared with  $13.2 \pm 2.9$  % without DPPC, as shown in Table 3. The large difference in respirable fraction between the DPPC and non-DPPC particles is at least in part attributed to reduced particle-particle interaction due to the use of DPPC.

In order to estimate the theoretical respirable fraction (RF) of the microspheres, and compare it with experimentally measured *in vitro* and *in vivo* RF's, size distribution measurements were analyzed to determine the percentage of particles (by mass) of each type (DPPC and non-DPPC) that were within the theoretical respirable size range (*i.e.*,  $d_{\text{resp}}$  Table 2). As shown in Table 3, a higher percentage of particles made with DPPC are expected to be respirable compared with non-DPPC particles (63 to 51%, respectively). This theoretical respirable fraction is based on the mass fraction of microspheres with diameters in the respirable size range,  $d_{\text{resp}}$  as defined by Eq. (2), and therefore takes into account the different sizes and densities of the two batches of microspheres.

**Table 3. Comparison of Microparticle Aerosolization Properties *In Vitro***

Sample	Theoretical Respirable Fraction (i.e., Mass % of microspheres in Respirable Size Range) <sup>a</sup>	Measured Respirable Fraction (% <i>In Vitro</i> ) <sup>b</sup>
microspheres without DPPC	51 ± 6	13.2 ± 2.9
microspheres with DPPC	63 ± 2	37.0 ± 2.1

<sup>a</sup>Based on theoretical respirable size range ( $d_{resp}$ , Table 2) and size distribution analyses.

<sup>b</sup>Measured using an Andersen Mark I Cascade Impactor.

To determine whether agglomeration forces during particle aerosolization from the Spinhaler device might be playing a role even after the particles enter the impactor system (i.e., primarily non-DPPC particles remain agglomerated in the inspired stream, resulting in deposition in the first two impactor stages: stages 0 and 1), *in vivo* aerosolization experiments were performed in which particles were permitted to fall by gravity into the inspiration stream of a Harvard ventilator system joined with the trachea of an anesthetized rat. In this model, approximately 63% of the inhaled DPPC-PLGA particles deposit in the airways and distal lung regions, whereas 57% of the non-DPPC particles are able to penetrate beyond the trachea in the lungs. These respirable fractions are much nearer to the predicted respirable fractions based upon particle diameter and mass density (Table 3).

Particle aggregation thus is less with DPPC-containing PLGA particles than without DPPC, even though the particles are of similar size and surface morphological features. The use of DPPC thus appears to reduce interparticle attractions, such as van der Waals and electrostatic attractions. It is also possible that the presence of DPPC reduces

moisture absorption which may cause particle-particle interaction by capillary forces.

In addition to the biocompatibility features of DPPC and improvement of surface properties of microspheres for aerosolization, it is possible that the release of DPPC from the slow-eroding PLGA microspheres in the alveolar region of the lungs can more effectively insure the maintenance of normal surfactant fluid composition thereby minimizing the possibility of local toxic side effects. The alveolar surfactant fluid layer is, on average, 10 nm thick (Weibel, E.R., *Morphometry of the Human Lung*, New York: Academic Press (1963)).

**Example 4: Fabrication of PLGA Microspheres by Spray  
Drying which Encapsulate a Model High  
Molecular Weight Drug, FITC-Dextran.**

Microspheres were made by spray drying using a variety of polymeric carriers with and without the incorporation of DPPC. The results are summarized in Table 4.

**Table 4. Characterization of Spray Dried Microparticulates**

Sample	Mass-Mean (True) Diameter, ( $\mu$ m)	DPPC Load ( $\mu$ g/mg spheres) and Efficiency (%)	FITC- Dextran Loading Efficiency, (%)	% of Surface Coated with DPPC by ESCA
R206+DPPC	5.4	<i>a</i>	54.9	<i>a</i>
R206 - DPPC	4.4	-	64.8	-
RG503+DPPC	2.0	62.8	65.2	46.5%
RG503 - DPPC	3.0	-	78.2	-
RG506+DPPC	4.3	89.1	62.7	42-62%
RG506 - DPPC	<i>b</i>	-	100	-

<sup>a</sup>Not Determined

<sup>b</sup>No reliable determination because the powder was highly aggregated.

Aerosolization properties of the microspheres also were examined, as shown in Table 5. Microspheres made by spray drying with and without DPPC have similar size distributions (Table 5) and mass densities ( $0.49 \pm 0.04$  g/cc). However, the aerosolization performance of spray-dried aerosols made with and without DPPC is markedly different. Figure 3 shows that the fraction of low-molecular-weight PLGA RG503 microparticles that are aerosolized from the dry powder inhaler (i.e., the % of particles that leave the DPI upon simulated inhalation, defined as the DPI Efficiency) is 70.4 % when the particles are made with DPPC compared with only 46.8 % for particles made without DPPC. Furthermore, the deposition of all types of polymer microparticles following aerosolization into an Andersen impactor is greatly improved using DPPC-coated particles (Table 5). Without the use of DPPC,  $\leq 2$  % of the particles aerosolized reach the latter stages of the impactor (those corresponding to the respirable fraction, stages 2-Filter). On the other hand, a maximum of 25.6% of DPPC-coated microspheres reach stages 2-Filter, as shown in Figure 4. Higher respirable fractions may be obtained with particles that contain low molecular weight drugs that are soluble in methylene chloride and therefore do not require the use of water during their preparation.

**Table 5. Summary of Aerosolization Data of microspheres Prepared by Spray Drying with or without DPPC**

Sample	% Aerosolized Particles that reach stages 1 - Filter	% Aerosolized Particles that reach stages 2 - Filter	% Aerosolized Particles that reach stages 3 - Filter	DPI Efficiency
R206 + DPPC	$40.4 \pm 8.4$	$25.6 \pm 2.3$	$18.0 \pm 2.7$	$38.6 \pm 3.7$
R206 - DPPC	$7.4 \pm 2.1$	$1.8 \pm 0.5$	$1.1 \pm 0.3$	$41.0 \pm 4.8$
RG503 + DPPC	$36.0 \pm 9.2$	$14.7 \pm 1.53$	$10.4 \pm 0.46$	$70.4 \pm 2.4$
RG503 - DPPC	$3.3 \pm 0.6$	$2.1 \pm 0.3$	$2.0 \pm 0.3$	$46.8 \pm 8.0$
RG506 + DPPC	$13.7 \pm 9.1$	$7.1 \pm 4.1$	$4.1 \pm 2.5$	$76.6 \pm 8.4$
RG506 - DPPC	$1.8 \pm 0.6$	$1.6 \pm 0.6$	$1.4 \pm 0.7$	$74.0 \pm 7.2$

R206 = PLA, molecular weight approximately 100,000.

RG503 = PLGA 50:50, molecular weight approximately 34,000.

RG506 = PLGA 50:50, molecular weight approximately 100,000.

**Example 5: Fabrication of Estradiol-Containing Lactose:DPPC Particles.**

Materials and Methods: A Niro Atomizer Portable Spray Dryer (Model #68) was used for all of the following Examples. Compressed air with variable pressure ran a rotary atomizer located above the dryer. Liquid feed with varying rate was pumped continuously by an electronic metering pump (LMI, model #A151-192s) to the atomizer. Both inlet and outlet temperatures can be measured and controlled manually. A container was tightly attached to the cyclone to collect the spray dried powder product.

Estradiol-containing particles were prepared to illustrate the preparation of large porous particles that contain a relatively large drug fraction by weight. Estradiol particles of standard mass density (greater than 0.4 g/cc) can be made in various ways. In this example, the particles included 30%  $\beta$ -estradiol, 62% lactose and 8% DPPC by weight. The lactose was dissolved in deionized water and the estradiol and DPPC were dissolved in 95% v/v ethanol. The two solutions were combined to form an 85% v/v ethanol solution. The total concentration of powdered starting materials in the solution was 3.25% w/v. The solution was spray dried under the following condition: The inlet temperature was 160°C; the outlet temperature was 95°C; the atomization pressure was 2 kp/cm<sup>2</sup> (28.45 psi); and the feed rate was 34 ml/min. The resulting spray dried powder had a tap (mass) density of 0.46 g/ml. The mean diameter based on volume, as measured using a Microtrac particle sizer, was 3.5  $\mu$ m, thus giving an aerodynamic diameter of 2.4  $\mu$ m.

In another example, estradiol particles of standard mass density (about 1 g/cc) were prepared by spray drying a solution containing 70% estradiol and 30% DPPC with a total powder concentration of 1.9% w/v in 85% v/v ethanol. The spray dryer was operated under the following conditions; the inlet temperature was 150°C, the outlet temperature was 85°C, the atomization pressure was 1 kp/cm<sup>2</sup> (14.22 psi), and the feed rate was 30 ml/min. The particles produced had a tap density of 0.62

g/ml and a mean diameter of 6  $\mu\text{m}$ , thus giving an approximate aerodynamic diameter of 4.7  $\mu\text{m}$ .

In order to produce light, porous particles, many combinations of operating conditions and powder compositions were tested. Another example of the preparation of low density particles was as follows; A solution of 90%  $\beta$ -estradiol and 10% DPPC by weight in 95% ethanol was prepared. The solution was then combined with deionized water to make a solution of 85% ethanol. The total powder concentration was 1.1% w/v. The operating conditions were as follows; the inlet temperature was 110°C, the outlet temperature was 85°C, the atomization pressure was 1  $\text{kp}/\text{cm}^2$  (14.22 psi), and the feed rate was 30 ml/min. The yield was 53.0%. The resulting powder was very flowable, and was made up of particles possessing irregular shapes and rough surfaces, as viewed by a SEM (scanning electron microscope). The mean diameter, determined by the Microtrac, based on volume was 6  $\mu\text{m}$ . The tap density was 0.28, thus giving an approximate aerodynamic diameter of 2.6 microns, which falls within the desired range of between one and five microns.

**Example 6: Preparation of Lactose:DPPC Carrier Particles.**

"Carrier" particles can be created to mimic drug-carrying particles with similar excipient concentrations. Case studies of four carrier particles are discussed below, followed by two examples of adding small concentrations of drug to the carrier particle. In this example, a small weight percentage of drug in the particle is considered to be less than 20% of the total powder weight.

Carrier particles with standard mass density can be prepared via several methods. An example is the following formulation. Solution of lactose in deionized water and DPPC in ethanol were combined to provide a solution containing relative ratios of 67% lactose and 33% DPPC by weight in 85% ethanol, with the total powder concentration in the solution of about 0.1% w/v. The solution was spray dried under the following conditions; the inlet temperature was 200°C; the outlet temperature was



119°C; the atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The yield of this run was 29.3%. The resulting spray dried powder had a tap (mass) density of 0.41 g/ml and a mean diameter by volume average estimated from an SEM of 2.5 μm, thus giving an approximated aerodynamic diameter of 1.6 microns, which is within the desired range of between one and five microns.

Powder composition, powder concentration, solvent composition and spray drier operating conditions are some of the factors which can be varied in order to produce light, porous carrier particles. Large, porous particles can be made that have a donut-like morphology. Such particles can be prepared, for example, by preparing a solution that includes 33% human albumin, 33% lactose, and 33% DPPC by weight. The human albumin and lactose was dissolved in deionized water and the DPPC was dissolved in 95% ethanol. The two solutions were combined to yield an 85% ethanol solution. The total powder concentration was about 0.1% w/v. The solution was spray dried under the following conditions; the inlet temperature was 110°C; the outlet temperature was 60°C; the atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The yield from this run was 38.5%. The tap (mass) density of the resulting particles was 0.16 g/ml, and the size of this particle on the coulter counter is 7.6 μm, thus giving an approximate aerodynamic diameter of 3.0 μm. (Note: The volume average sizes approximated from the SEM and those determined by the Coulter Counter can be considered equivalent.)

#### **Example 7: Preparation of Albumin:Lactose:DPPC Particles.**

Another type of large, porous particles looks similar to a dried grape. Particles with this type of morphology can be prepared, for example, by spray drying a solution that contains 20% human albumin, 20% lactose, and 60% DPPC by weight. The human albumin and lactose were dissolved in deionized water and the DPPC was dissolved in 95% ethanol. The two solutions were combined to form an 85% ethanol solution. The total powder concentration was about 0.1% w/v. The

solution was spray dried under the following conditions; the inlet temperature was 110°C; the outlet temperature was 60°C; the atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The yield was 45.0%. The tap (mass) density of this particle is 0.05 g/ml, and the approximate volume-average size of this particle from the SEM was 7 μm, thus giving an approximate aerodynamic diameter of 1.6 μm. Aerosolization studies of this particle yielded the following results; aerosolized fraction was 58.5%; respirable fraction was 26.6%, and respirable fraction of inhaled aerosol was 43.8%.

**Example 8: Preparation of Albumin:Lactose:DPPC Particles.**

Various methods can be used to increase the size of the particles. The particles prepared in this example had roughly the same morphology as those in Example 7, but had a larger particle size. The particles were prepared as follows: A solution of 20% human albumin, 20% lactose, and 60% DPPC by weight was spray dried. The human albumin and lactose were dissolved in deionized water and the DPPC was dissolved in 95% ethanol. The two solutions were combined to form an 85% ethanol solution. The total powder concentration was about 0.2% w/v. The solution was spray dried under the following conditions; the inlet temperature was 110°C; the outlet temperature was 51°C; the atomization pressure was 2 kp/cm<sup>2</sup> (28.48 psi); and the feed rate was 66 ml/min. The yield from this run was 48.6%. The tap (mass) density of the resulting particles was 0.04 g/ml, and the approximate volume-average size of the particles from the SEM was 10 μm, thus giving an approximate aerodynamic diameter of 2.0 microns.

**Example 9: Spray Drying of Insulin:Albumin:Lactose:DPPC Particles.**

This example demonstrates that adding less than 20% drug by weight has little change on the particle morphology, size, tap density, and aerosolization characterizations. For example, human insulin was added at a concentration of about 2% by weight of the particles in Example 7. The particles were prepared by spray drying a solution of 2% human

insulin, 19% human albumin, 19% lactose, and 60% DPPC by weight.

The human insulin, human albumin and lactose were dissolved in deionized water and the DPPC was dissolved in 95% ethanol. The solubility of human insulin in the deionized water was increased by

5 adding a few drops of NaOH (5g NaOH/100 ml deionized water) until the insulin went into solution. The two solutions were combined to form an 85% ethanol solution. The total powder concentration was about 0.1% w/v. The solution was spray dried under the following conditions; the inlet temperature was 110°C; the outlet temperature of 61°C; the  
10 atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The yield from this run was 51.1%. The tap (mass) density of the resulting particles was 0.05 g/ml and the approximate volume-average size of this particle from the SEM was 6.5 μm, thus giving an approximate aerodynamic diameter of 1.5 μm. The morphology of the  
15 particles was very similar to the particles in Example 7. Aerosolization studies of these particles yielded the following results: the aerosolized fraction was 45.0%; the respirable fraction was 15.0%; the respirable fraction of the inhaled aerosol was 58.3%.

**Example 10: Preparation of Albuterol Particles.**

20 Albuterol particles with a relatively small amount of drug by weight were also prepared. In this example, particles were prepared according to the procedure in Example 6, except that 4% albuterol by weight of the particle was added. The particles were formed by spray drying a solution containing 4% albuterol, 33% human albumin, 33%  
25 lactose, and 33% DPPC by weight. The albuterol, human albumin and lactose were dissolved in deionized water and the DPPC was dissolved in 95% ethanol. The solutions were combined to form an 85% ethanol solution. The total powder concentration was about 0.1% w/v. The solution was spray dried under the following conditions; the inlet  
30 temperature was 110°C; the outlet temperature was 60°C; the atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The yield from this run was 46.8%. The tap (mass) density of the resulting

particles was 0.15 g/ml and the size of the particles as measured on a Coulter counter was 7.2  $\mu\text{m}$ , thus giving an approximate acrodynamic diameter of 2.8  $\mu\text{m}$ .

**Example 11: Preparation of Sustained Release Insulin Particles.**

5           Sustained release of insulin out of the particles was achieved by rendering the insulin insoluble. Insulin was dissolved in ultrapure water (0.02% w/v). Protamine was then added (in the proportion insulin/protamine 5/1 w/w) to form an insulin/protamine complex. The formation of the insulin/protamine complex causes the insulin to  
10 precipitate. The complex was dissolved by raising the pH to about 5 with HCl so that the solution could be spray dried. Lactose was then added to the solution. The aqueous solution was then mixed with a 95% v/v ethanol solution containing DPPC. The final concentration of each excipient in the 85% v/v solution was insulin/protamine/lactose/DPPC  
15 2/0.4/37.6/60% w/v. The solution was spray dried under the following conditions; the inlet temperature was 110°C; the outlet temperature was 60°C; the atomization pressure was 3 kp/cm<sup>2</sup> (42.72 psi); and the feed rate was 40 ml/min. The ability of the particles to provide sustained release *in vitro* was evaluated. Particles suspended in phosphate buffer  
20 saline at pH 7.4 released less than 10% of the incorporated insulin after 5 hours.

**Example 12:           Preparation of Insulin:Protamine:Zinc Complexes.**

25           Particles containing a complex of insulin/protamine/zinc were prepared according to the process in Example 11. The concentration of each excipient in the ethanol/water (85:15 % v/v) solution was insulin/protamine/zinc chloride/lactose/DPPC 2:0.6:0.25:32.4:60 (% w/v). The solution was spray dried under the same conditions in Example 11. The formulation was also shown to provide sustained  
30 release of insulin *in vitro*.

The particles (8 mg) were inhaled into the lungs of rats using the procedures described in Edwards, et al. (Science, 276, 1868 (1997)). For

comparison purposes, the particles were also injected subcutaneously and non-sustained insulin particles of identical insulin content (without protamine or zinc) were injected subcutaneously and inhaled. Figure 5 shows the plasma concentration per unit time for insulin administered via the various modes of administration. The inhaled protamine/zinc particles resulted in sustained high serum insulin concentrations for at least 24 hours, in contrast to particles without protamine or zinc, which released insulin in less than approximately 5 hours.

Therapeutics other than insulin can be complexed in the same manner and included in the particles. Proteins having an isoelectric point (pI) lower than the physiological pH of 7.4 as insulin (pI=5.3) can be precipitated in the same manner using protamine (e.g., growth hormone, pI=4.9). Proteins having a pI higher than pH of 7.4 (e.g., LHRH, calcitonin) can be precipitated using a negatively charged compound (e.g., dextran-sulfate) or by adding an appropriate salt. This approach can be extended to drugs (e.g., heparin) other than therapeutic proteins as well.

#### **Example 13: Preparation of Sustained Release Albuterol Particles.**

Albuterol particles were prepared to evaluate the sustained release of a hydrophilic molecule from particles. The albuterol-containing particles were prepared as described in Example 7, reducing the percentages of lactose and albumin (while keeping the ratio equal) and adding cholesterol (of varying percentages; 6, 8, 10, 25%) and albuterol (4%). The addition of cholesterol led to an increasingly slower release of albuterol, as shown in Figure 6. Albuterol concentration was measured using a UV spectrophotometer. The data shown in Figure 6 demonstrates that cholesterol can be incorporated into particles to provide sustained albuterol release. Similar results can be achieved by increasing the DPPC concentration beyond 60%.

#### **Example 14: Release Properties of Albumin:DPPC:Lactose:Albuterol Particles.**

Particles (mean diameter 10 $\mu$ m, tap density 0.06 gram<sup>3</sup>) were prepared particles as described in Example 7 with 60% DPPC, 18%

albumin, 18% lactose, and 4% albuterol to demonstrate that sustained release of a hydrophilic molecule such as albuterol can also be achieved without cholesterol. The *in vitro* release of albuterol is shown in Figure 7 both for this formulation and a non-sustained release formulation that included only lactose (96%) and albuterol (4%). Even without cholesterol, the release of the albuterol was sustained for nearly 24 hours.

Particles (5 mg, i.e. 200  $\mu$ g albuterol dose) were administered to guinea pigs using the procedures in Example 12 to demonstrate that the sustained release albuterol particles could produce sustained bronchodilation. The animals were administered carbachol prior to measuring airway resistance. Airway resistance was monitored using a Buxco system. Airway resistance dropped sharply following inhalation of the large porous particles (Figures 7 and 8) and remained at statistically low levels for approximately 1 day ( $n = y$ ).

"Placebo" particles (60% DPPC, 20% albumin, 20% lactose) prepared as described in Example 11 were also administered. Airway resistance following carbachol challenge was measured at eight hours following inhalation and 15 hours following inhalation. The airway resistance was  $1.0 \pm 0.3$  and  $1.0 \pm 0.2$  cm H<sub>2</sub>O/ml/sec., proving that the bronchodilation observed in Figure 8 was due to slow albuterol release.

Slow albuterol release has also been achieved *in vitro* using particles prepared by the methods of Example 7 with 10% DPPC, 86% albumin, and 4% albuterol. However particles prepared with 10% DPPC, 43% albumin, 43% lactose, and 4% albuterol did not display significantly slower albuterol release *in vitro*, indicating that for relatively low DPPC content, high albumin content is favorable for sustained albuterol release.

These examples demonstrate that by choosing the composition of the spray dried materials and by varying the spray drying parameters, the aerodynamic properties of the inhaled particles can be effectively controlled. More specifically, the composition of the spray dried material especially affects the density and shape of the particles while the spray

drying parameters have a stronger affect on their size. For instance, increasing the proportion of lactose in the particles make the particles heavier, while increasing the albumin or dipalmitoyl phosphatidylcholine (DPPC) content makes them lighter. Increasing DPPC content also  
5 increases the particle size. Nevertheless, when a relatively small proportion of drug is incorporated in the particles, the characteristics of the particles remain relatively unaffected. Decreasing the inlet temperature largely increases the size of the particles without greatly affecting their tap density. Increasing the feed rate and decreasing the  
10 pressure of the compressed air both tend to increase the size of the particles without greatly affecting their density. However, these effects are smaller than those of the temperature.

We claim:

1. A particulate composition for drug delivery to the pulmonary system comprising:  
biodegradable particles incorporating a therapeutic agent and a material selected from the group consisting of surfactant and a molecule having a charge opposite to the charge of the therapeutic agent and forming a complex thereto, wherein the particles have a tap density less than  $0.4 \text{ g/cm}^3$  and a mean diameter between  $5 \text{ }\mu\text{m}$  and  $30 \text{ }\mu\text{m}$  effective to yield an aerodynamic diameter of the particles of between approximately one and five microns.
2. The composition of claim 1 wherein the aerodynamic diameter of the particles is between approximately one and three microns.
3. The composition of claim 1 wherein at least 50% of the particles have a mean diameter between  $5 \text{ }\mu\text{m}$  and  $15 \text{ }\mu\text{m}$  and a tap density less than  $0.1 \text{ g/cm}^3$ .
4. The composition of claim 1 further comprising a pharmaceutically acceptable carrier for administration to the lungs.
5. The composition of claim 1 wherein the particles comprise a biodegradable polymer.
6. The composition of claim 1 wherein the particles comprise a complex of charged molecules and a surfactant.
7. The composition of claim 1 wherein the particles comprise an excipient.
8. The composition of claim 1 wherein the particles have an irregular surface structure.
9. The composition of claim 1 wherein the surfactant is coated on the surface of the particle.
10. The composition of claim 1 wherein the surfactant is incorporated within and on the surface of the particle.
11. The composition of claim 1 wherein the therapeutic agent is selected from the group consisting of proteins, polysaccharides, lipids, nucleic acids and combinations thereof.



12. The composition of claim 1 wherein the therapeutic agent is selected from the group consisting of nucleotides and oligonucleotides.

13. The composition of claim 11 wherein the therapeutic agent is selected from the group consisting of insulin, calcitonin, leuprolide and albuterol.

14. The composition of claim 1 wherein the surfactant is selected from the group consisting of a fatty acid, a phospholipid, and a block copolymer.

15. The composition of claim 14 wherein the surfactant is a phosphoglyceride.

16. The composition of claim 14 wherein the surfactant is L- $\alpha$ -phosphatidylcholine dipalmitoyl.

17. The composition of claim 1 wherein the agent is a charged species and is present as a complex with an oppositely charged species.

18. The composition of claim 17 wherein the agent is hydrophilic and is present as a complex with a hydrophobic moiety.

19. A method for drug delivery to the pulmonary system comprising:

administering to the respiratory tract of a patient in need of treatment an effective amount of biodegradable particles incorporating a therapeutic agent and a molecule selected from the group consisting of surfactant and a molecule having a charge opposite to the charge of the therapeutic agent and forming a complex thereto,

wherein the particles have a tap density less than about 0.4 g/cm<sup>3</sup> and a mean diameter of between 5  $\mu$ m and 30  $\mu$ m effective to yield an aerodynamic diameter of the particles of between approximately one and five microns.

20. The method of claim 19 wherein the aerodynamic diameter of the particles is between approximately one and three microns.

21. The method of claim 19 wherein at least 50% of the administered particles have a mean diameter between 5  $\mu$ m and 15  $\mu$ m.

22. The method of claim 19 wherein at least 50% of the administered particles have a mean diameter between 5  $\mu\text{m}$  and 15  $\mu\text{m}$  and a tap density of less than about 0.1 g/cm<sup>3</sup>.
23. The method of claim 19 wherein the particles comprise a biodegradable polymer.
24. The method of claim 19 wherein the particles comprise a complex of charged molecules and surfactant.
25. The method of claim 19 wherein the particles comprise an excipient.
26. The method of claim 23 wherein the particles have an irregular surface structure and have surfactant incorporated on or within the particle.
27. The method of claim 19 for delivery to the alveolar zone of the lung wherein at least 90% of the particles have a mean diameter between about 9  $\mu\text{m}$  and 11  $\mu\text{m}$  and a tap density less than 0.1 g/cm<sup>3</sup>.
28. The method of claim 19 wherein the therapeutic agent is selected from the group consisting of proteins, polysaccharides, lipids, nucleic acids and combinations thereof.
29. The method of claim 19 wherein the therapeutic agent selected from the group consisting of nucleotides and oligonucleotides.
30. The method of claim 28 wherein the therapeutic agent is selected from the group consisting of insulin, calcitonin, leuprolide and albuterol.
31. The method of claim 19 wherein the particles are administered in combination with a pharmaceutically acceptable carrier for administration to the respiratory tract.
32. The method of claim 19 wherein the surfactant is selected from the group consisting of a fatty acid, a phospholipid, and a block copolymer.
33. The method of claim 32 wherein the surfactant is a phosphoglyceride.

34. The method of claim 32 wherein the surfactant is L- $\alpha$ -phosphatidylcholine dipalmitoyl.
35. The method of claim 32 wherein the surfactant is coated on the surface of the particle.
36. The method of claim 32 wherein the surfactant is incorporated within and on the surface of the particle.
37. The method of claim 19 wherein the agent is a charged species and is present as a complex with an oppositely charged species.
38. The method of claim 19 wherein the agent is hydrophilic and is present as a complex with a hydrophobic moiety.

## AMENDED CLAIMS

[received by the International Bureau on 30 June 1998 (30.06.98);  
original claims 1-38 replaced by amended claims 1-31 (4 pages)]

1. A particulate composition for drug delivery to the pulmonary system comprising biocompatible particles incorporating a therapeutic agent and a surfactant, wherein the particles have a tap density less than  $0.4 \text{ g/cm}^3$  and a mean diameter between  $5 \mu\text{m}$  and  $30 \mu\text{m}$  effective to yield an aerodynamic diameter of the particles of between approximately one and five microns.
2. The composition of claim 1 or 17 wherein the aerodynamic diameter of the particles is between approximately one and three microns.
3. The composition of claim 1 or 17 wherein at least 50% of the particles have an aerodynamic diameter between three  $\mu\text{m}$  and  $5 \mu\text{m}$  and a tap density less than  $0.2 \text{ g/cm}^3$ .
4. The composition of claim 1 or 17 further comprising a pharmaceutically acceptable carrier for administration to the lungs.
5. The composition of claim 1 or 17 wherein the particles comprise a biodegradable polymer.
7. The composition of claim 1 or 17 wherein the particles comprise an excipient.
8. The composition of claim 1 or 17 wherein the particles have an irregular surface structure.
9. The composition of claim 1 or 17 wherein the surfactant is coated on the surface of the particle.
10. The composition of claim 1 or 17 wherein the surfactant is incorporated within and on the surface of the particle.
11. The composition of claim 1 or 17 wherein the therapeutic agent is selected from the group consisting of proteins, polysaccharides, lipids, nucleic acids and combinations thereof.

12. The composition of claim 1 or 17 wherein the therapeutic agent is selected from the group consisting of nucleotides and oligonucleotides.

13. The composition of claim 11 wherein the therapeutic agent is selected from the group consisting of insulin, calcitonin, leuprolide, granulocyte colony-stimulating factor, parathyroid hormone-related peptide, somatostatin, testosterone, progesterone, estradiol, nicotine, fentanyl, norestherone, clonidine, scopolomine, salicylate, cromolyn sodium, salmeterol, formeterol, valium and albuterol.

14. The composition of claim 1 or 17 wherein the surfactant is selected from the group consisting of a fatty acid, a phospholipid, and a block copolymer.

15. The composition of claim 14 wherein the surfactant is a phosphoglyceride.

16. The composition of claim 14 wherein the surfactant is L- $\alpha$ -phosphatidylcholine dipalmitoyl.

17. A composition for delivery to the pulmonary system comprising particles formed of a therapeutic agent and a surfactant, wherein the surfactant constitutes greater than 60% of the total weight of the particles.

18. A particulate composition for drug delivery to the pulmonary system comprising:

biocompatible particles incorporating a therapeutic agent which is a charged species and a molecule having a charge opposite to the charge of the therapeutic agent and forming a complex thereto.

19. The composition of claim 18 wherein the particles have a tap density less than 0.4 g/cm<sup>3</sup> and a mean diameter between 5  $\mu$ m and 30  $\mu$ m effective to yield an aerodynamic diameter of the particles of between approximately one and five microns.

20. The composition of claim 18 wherein the agent is hydrophilic, the molecule includes a hydrophobic moiety, and the agent and molecule form a complex.
21. The composition of claim 18 wherein the therapeutic agent is negatively charged and the molecule forms a lipophilic complex.
22. The composition of claim 18 wherein the therapeutic agent is selected from the group consisting of insulin, calcitonin, leuprolide, granulocyte colony-stimulating factor, parathyroid hormone-related peptide, somatostatin, testosterone, progesterone, estradiol, nicotine, fentanyl, norestherone, clonidine, scopolomine, salicylate, cromolyn sodium, salmeterol, formeterol, valium and albuterol.
23. The composition of claim 18 wherein the charged molecule is protamine.
24. The composition of claim 18 wherein the therapeutic agent is insulin, the molecule is protamine, and the complex further comprises zinc.
25. A composition for delivery to the pulmonary system comprising a therapeutic agent selected from the group consisting of testosterone, progesterone, estradiol, and norestherone.
26. The composition of claim 25 wherein the therapeutic agent is estradiol.
27. A composition for sustained release in the lung comprising insulin or albuterol.
28. The composition of claim 27 comprising a complex of insulin, protamine and zinc.
29. The composition of claim 27 providing sustained serum insulin concentrations for at least 24 hours.

30. A method for drug delivery to the pulmonary system comprising:

administering to the respiratory tract of a patient in need of treatment an effective amount of the compositions of any of claims 1-29.

31. A method for manufacture of a medicament for delivery to the pulmonary system comprising preparing the compositions of any of claims 1-29.

1/4

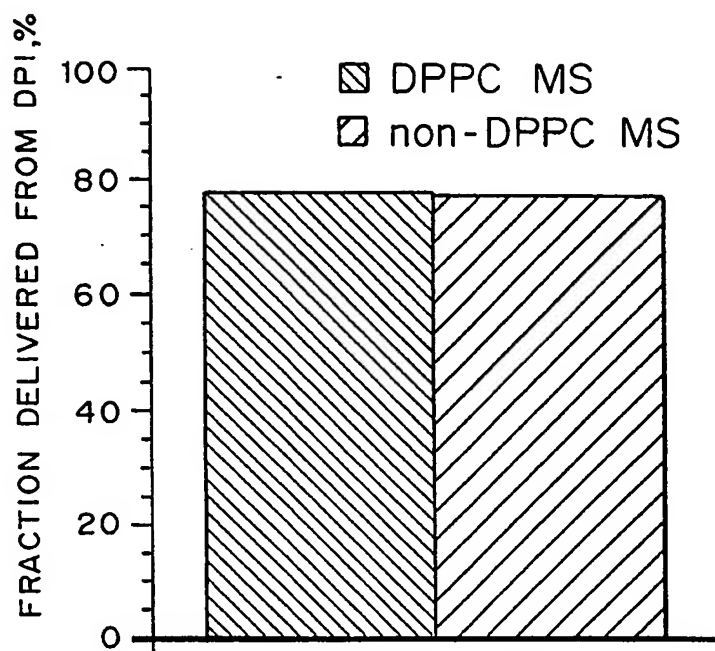


FIG. 1

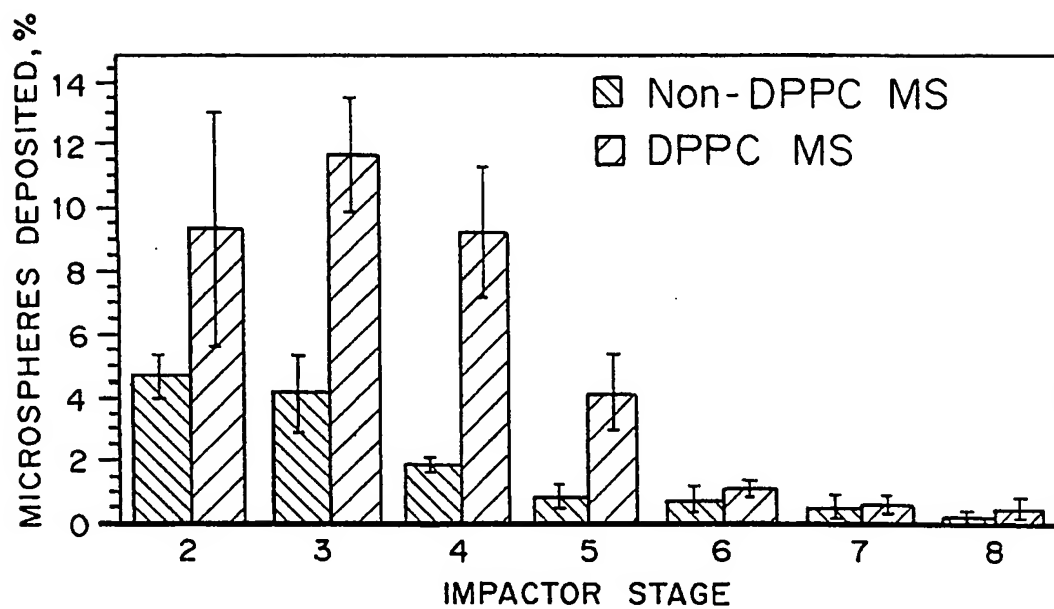


FIG. 2



2/4

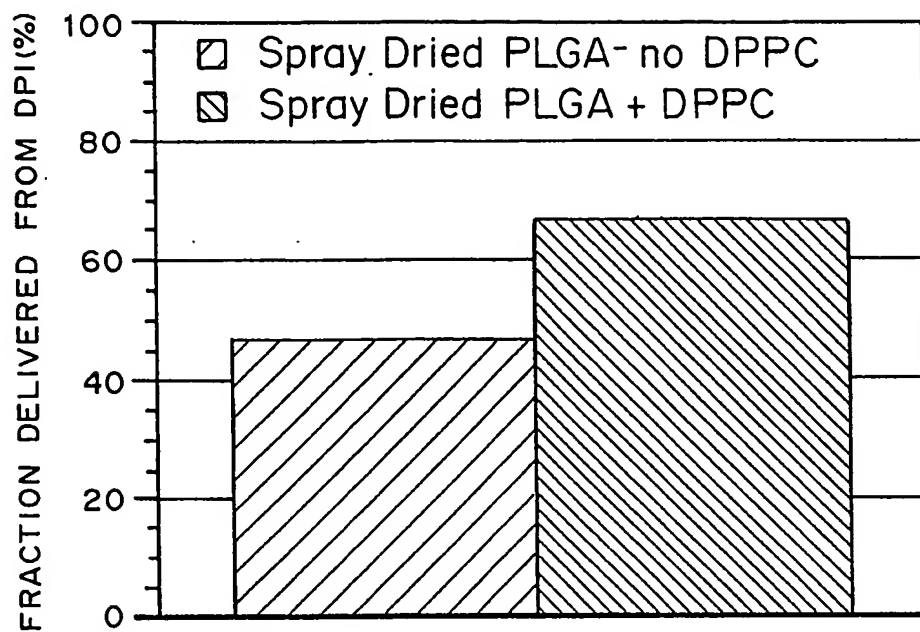


FIG. 3

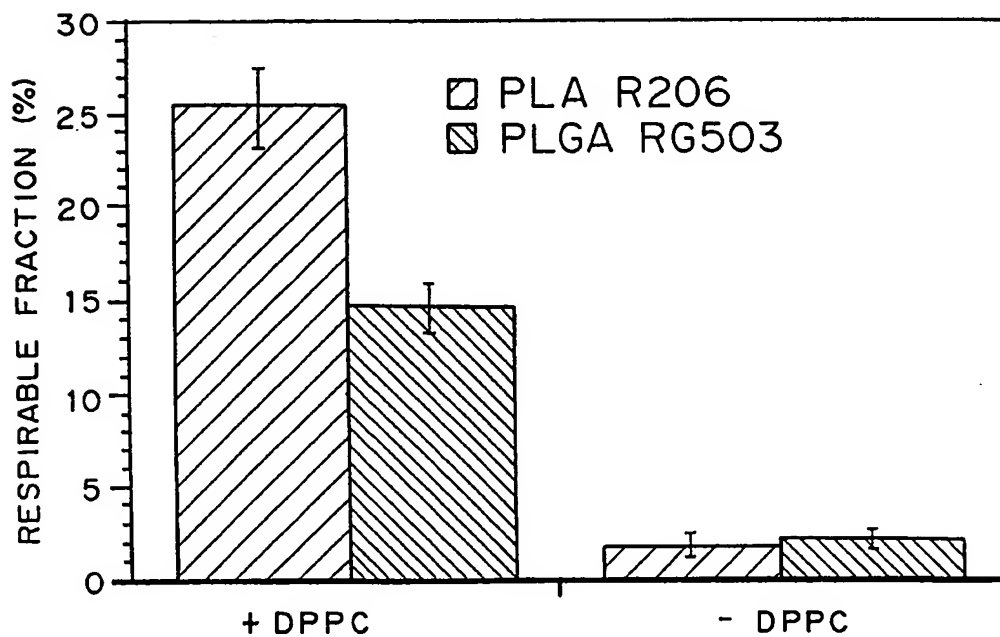


FIG. 4

3/4

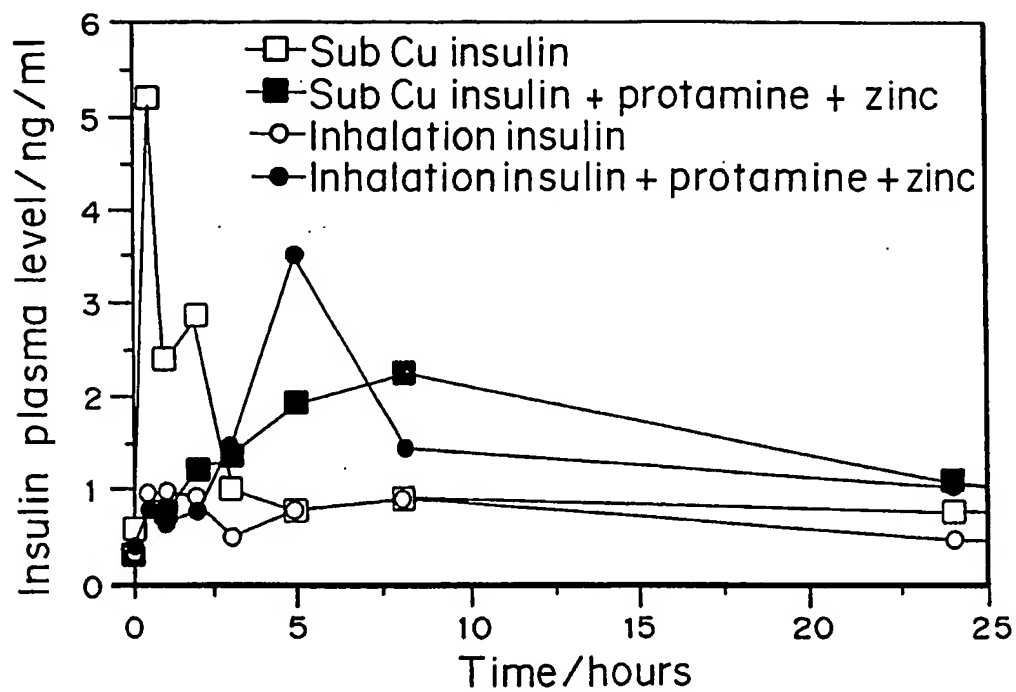


FIG. 5

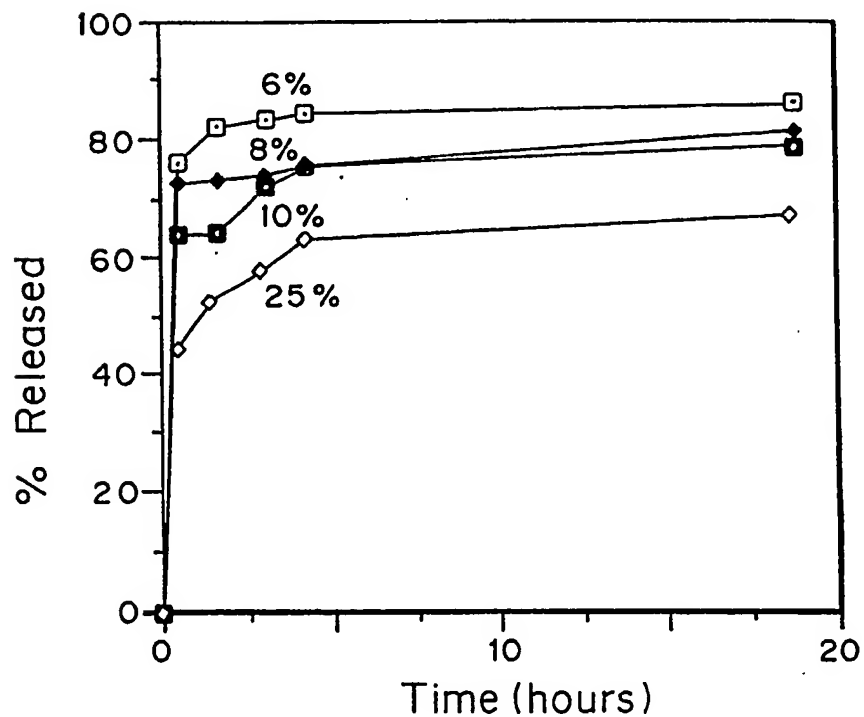


FIG. 6

4/4

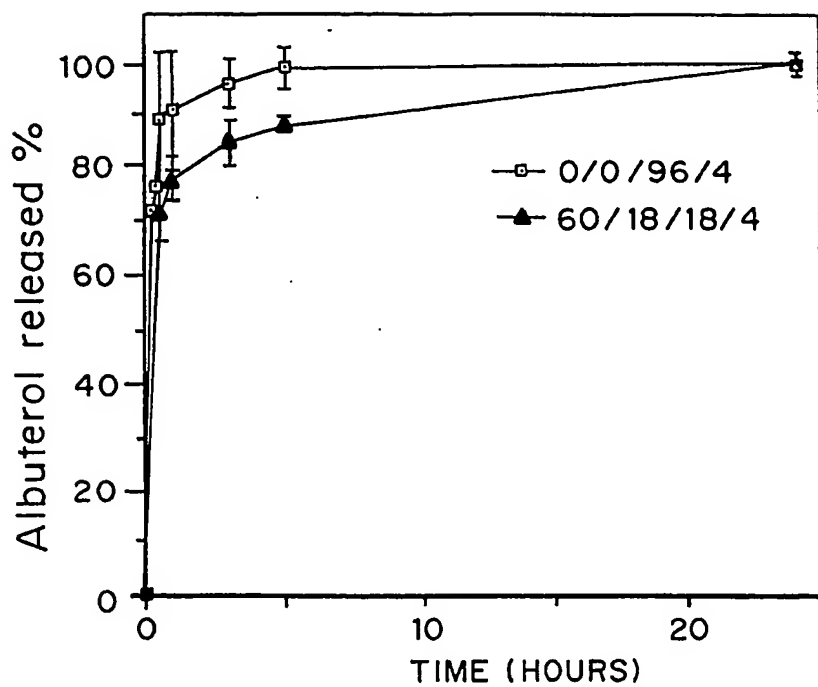


FIG. 7

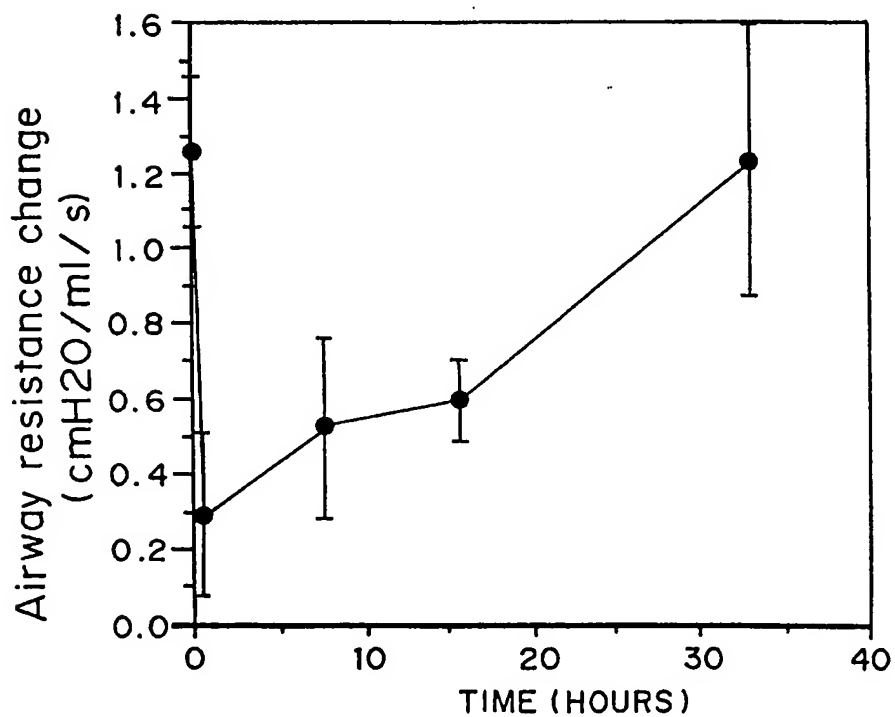


FIG. 8

# INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 97/20930

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 A61K9/12 A61K9/00 A61K9/16 A61K47/48 A61K47/14  
A61K38/28 A61K38/23 A61K38/09 A61K31/135

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 A61K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	J. HANES ET AL.: "Porous dry-powder PLGA microspheres coated with lung surfactant for systemic insulin delivery via the lung" PROC. INT. SYMP. CONTROLLED RELEASED BIOACT. MATER., no. 24th, 1997, DEPARTMENT OF CHEMICAL ENGINEERING, MASSACHUSETTS INSTITUTE OF TECHNOLOGY, CAMBRIDGE, MA, 02139, USA, pages 57-58, XP002061402 *cf. introduction, and on page 58, right col., "conclusions"* ---	1-38
X	US 5 306 483 A (MAUTONE ALAN J) 26 April 1994 *cf. abstract, col. 1, "background of the invention", col. 2, lines 5-26, col. 8, lines 4-23, ex. 2* ---	1-38
	-/--	



Further documents are listed in the continuation of box C.



Patent family members are listed in annex.

### \* Special categories of cited documents :

\*A\* document defining the general state of the art which is not considered to be of particular relevance

\*E\* earlier document but published on or after the international filing date

\*L\* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

\*O\* document referring to an oral disclosure, use, exhibition or other means

\*P\* document published prior to the international filing date but later than the priority date claimed

\*T\* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

\*X\* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

\*Y\* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

\*Z\* document member of the same patent family

Date of the actual completion of the international search

3 April 1998

Date of mailing of the international search report

30.04.98

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2  
NL - 2280 HV Rijswijk  
Tel. (+31-70) 340-2040, Tx. 31 651 epo.nl  
Fax: (+31-70) 340-3016

Authorized officer

Stoltner, A

# INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 97/20930

## C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP 0 510 731 A (ABBOTT LAB) 28 October 1992 *page 2, lines 35-40, lines 45-55, page 3, lines 31-46* ---	1-38
Y	WO 95 35097 A (UNIV NOTTINGHAM ;YEH MING KUNG; COOMBES ALAN GERALD ARTHUR (GB); J) 28 December 1995 *cf. abstract, page 5, lines 15-25, page 5, lines 22-28, page 10, first para.* ---	1-38
Y	EP 0 656 206 A (SCHERING CORP) 7 June 1995 *cf. abstract, page 3, lines 23-55, page 5, lines 41-55* ---	1-38
Y	EP 0 634 166 A (HOECHST AG) 18 January 1995 *cf. col. 2, lines 38-43, col. 3, lines 10-12, col. 4, lines 20-25* ---	1-38
Y	WO 96 09814 A (ANDARIS LTD) 4 April 1996 *cf. abstract, page 5, lines 20-30, page 13, lines 3-9, page 21, ex. 8, claims 1-4, 12 and 17* -----	1-38

# INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 97/20930

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
US 5306483 A	26-04-94	US 5174988 A	29-12-92
		EP 0607118 A	27-07-94
		WO 9101765 A	21-02-91
-----			
EP 0510731 A	28-10-92	US 4897256 A	30-01-90
		US 4851211 A	25-07-89
		AT 137963 T	15-06-96
		CA 1300009 A	05-05-92
		DE 3751811 D	20-06-96
		DE 3751811 T	28-11-96
		DE 3785570 A	27-05-93
		DE 3785570 T	18-11-93
		EP 0275404 A	27-07-88
		ES 2089301 T	01-10-96
		JP 2533586 B	11-09-96
		JP 63211237 A	02-09-88
-----			
WO 9535097 A	28-12-95	AU 2743695 A	15-01-96
		CA 2193203 A	28-12-95
		EP 0766554 A	09-04-97
		FI 965068 A	17-02-97
		GB 2303551 A	26-02-97
		JP 9510477 T	21-10-97
		NO 965403 A	16-12-96
-----			
EP 0656206 A	07-06-95	EP 0656207 A	07-06-95
		AT 134509 T	15-03-96
		AU 2017592 A	12-01-93
		CA 2111002 A	23-12-92
		CN 1067578 A	06-01-93
		CZ 9302714 A	13-07-94
		DE 69208660 D	04-04-96
		DE 69208660 T	11-07-96
		EP 0518600 A	16-12-92
		EP 0588897 A	30-03-94
		ES 2084360 T	01-05-96
		FI 935464 A	07-12-93
		HK 185596 A	11-10-96
		HU 67449 A	28-04-95
		JP 6511235 T	15-12-94

# INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 97/20930

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP 0656206 A	-	MX 9202750 A NO 934500 A OA 9868 A SK 140493 A WO 9222288 A US 5474759 A	31-12-92 09-12-93 15-08-94 05-10-94 23-12-92 12-12-95
EP 0634166 A	18-01-95	DE 4323636 A CA 2128034 A JP 7053353 A US 5663198 A	19-01-95 16-01-95 28-02-95 02-09-97
WO 9609814 A	04-04-96	AU 3530295 A CA 2199954 A CZ 9700924 A EP 0783298 A FI 971332 A NO 971438 A PL 319600 A	19-04-96 04-04-96 13-08-97 16-07-97 01-04-97 26-03-97 18-08-97